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Apport de la methode coiled tubing a l'augmentation de
la productivite d'un puits Tig 37 krechba petrolier

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DEDICATIONS

*I would like to dedicate this modest work to the people most dear
to my heart*

*To my mother, who always gives me hope to live and who has
never stopped*

never stopped praying for me.

*To my father, for his encouragement, his support, especially for
his*

*for his love and his sacrifice so that nothing hinders the progress
of my*

the progress of my studies.

To my dear brothers.

To all my big family,

To my teachers for their help.

To my best friends and all my classmates.

To all those whom I love and respect.

Thanks

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keywords

bbl/ft = barrels US per foot

bbl/min = barrels US per min

bbl/stroke = barrels US per stroke

BHP = bottom hole pressure

BOH = blow out preventer

TRSSV = Tubing-Retrievable Safety Valve

scf/bbl = Standard cubic feet/ barrels

PPE = personal protective equipment

MSDS = Material Safety Data Sheets

CTU Services = Coiled Tubing Unit Service

RIH \neq pooh

TRSV = Tubing-Retrievable Safety Valve

BPV = BACK PRESSURE VALVE PUMP

POOH = PULL-OUT-OF-HOLE

ABSTRACT

Interventions processes to deal with problems that stop production or hinder production efficiency, the term "well operations" refers to all the provisions applicable to the wells themselves and having as their object, on the one hand, knowledge of the evolution of the state of the wells or the deposit and, on the other hand The maintenance or the adaptation of the wells in order to remain in conditions of use as perfect as possible, out on a well are numerous and can be grouped together in measurement operations, maintenance operations and repackaging or recovery operations, they fall into two categories: light or heavy: Light interventions are cable work operations and pumping operations that based on light unit uses and heavy operations are coiled tubing, snubbing and work over operations that based on the use of multiple units and heavy units (Use drill rig on the work over operation and snubbing unit), Keywords: intervention, measurement, maintenance, wireline, coiled tubing, snubbing. workover.

RÉSUMÉ

Processus d'interventions pour faire face à des problèmes qui arrêtent la production ou entravent l'efficacité de la production, le terme « exploitation des puits » désigne l'ensemble des dispositions applicables aux puits eux-mêmes et ayant pour objet, d'une part, la connaissance de l'évolution de l'état des puits ou le gisement et, d'autre part La maintenance ou l'adaptation des puits afin de rester dans des conditions d'utilisation aussi parfaites que possible, hors sur un puits sont nombreuses et peuvent être regroupées en opérations de mesures, opérations de maintenance et de reconditionnement ou opérations de récupération, elles se répartissent en deux catégories : légères ou lourdes : les interventions légères sont des opérations de travail de câble et des opérations de pompage basées sur des utilisations d'unités légères et des opérations lourdes sont des unités lourdes (Use drill rig on the work over operation and snobbing unit), Mots clés : intervention, mesure, maintenance, filaire, coiled tubing, snubbing. retravailler.

ملخص

عمليات التدخل للتعامل مع المشكلات التي توقف الإنتاج أو تعيق كفاءة الإنتاج ، يشير مصطلح "عمليات البئر" إلى جميع الأحكام المطبقة على الآبار نفسها والتي يكون هدفها ، من ناحية ، معرفة تطور حالة الآبار أو الرواسب ، ومن ناحية أخرى ، صيانة أو تكييف الآبار من أجل البقاء في ظروف الاستخدام المثالية قدر الإمكان ، خارج البئر عديدة ويمكن تجميعها معاً في عمليات القياس وعمليات الصيانة وإعادة التعبئة أو عمليات الاسترداد ، فهي تنقسم إلى فئتين: الخفيفة أو الثقيلة: التدخلات الخفيفة هي عمليات عمل الكابلات وعمليات الضخ التي تعتمد على استخدامات الوحدات الخفيفة والعمليات الثقيلة ، وهي أنابيب ملفوفة ، وعزل ، والعمل على العمليات التي تعتمد على استخدام وحدات متعددة و الوحدات الثقيلة (استخدم جهاز الحفر في العمل فوق وحدة التشغيل والصدم) ، الكلمات الرئيسية: التدخل ، القياس ، الصيانة ، الكابلات السلكية ، الأنابيب الملتفة ، التنفيس بنج. انتهاء العمل

Intruduction General :

Despite the revolution in techniques used up to this point in drilling for the recovery of hydrocarbons the best known problem is the decrease in producio. a horizontal well was a ideal solution for field development, but due to the size of the reservoirs, drilling conventional new horizontal wells were not economically attractive.

Re-entry using boreholes. existing systems using Coiled Tubing Drilling (CTD) has been determined as one of the best options for the development of fields thanks to the equipment and

new techniques which confirm these advantages over conventional drilling.

A montage fast and shorter tripping times and generally result in higher production rates than those obtained using conventional overbalance drilling techniques. Coiled Tubing Drilling "CTD" is one of the newly introduced techniques on the field of Krechba deposit, it combines between the concepts of TC and conventional drilling, There are important differences between these two techniques.

The CTD offers several unique advantages and capabilities over the conventional drilling method, it has there are several drawbacks and usage limitations.

The aim of the work scale is to gain a good understanding of drilling with Coiled Tubing, its applications, its advantages as well as its limitations and to make a study to economize the drilling of CTD and the cleaning conventional.

For this we chose the well drilled in the same area of Krechba deposit fields, the Teg-37 wells conventionally using the Coiled Tubing unit Drilling.

ChapterI:
Description of Coiled Tubing

ChapterI: Description of Coiled Tubing 2**I.1.Intruduction :**

Coiled tubing involves pushing a pipe with downhole tools attached to its end into an oil or gas well to carry out work without disturbing, to complete the existing well. Although there are disadvantages, there are advantages that have encouraged its development.

I.2.History of Coiled Tubing :

Knowing a little about the history of coiled tubing can help you to understand current perceptions. Although coiled tubing has been in use for more than 30 years in oil and gas well operations, it is a “relatively” new type of well servicing equipment. As with any new technology, the early days had their share of failures as well as successes. Many times, fishing tools and prayers were required to get the tubing out of the hole. Given past performances of this type of well servicing unit, operators could not help having concerns when they had to run it in a well. However, times and coiled tubing are changing. When we look at the injectors that we previously used and the way the tubing was handled and spooled it becomes obvious that changes were necessary. The following in this manual will discuss each piece of equipment and point out why and how the equipment has changed to give us our modern coiled tubing units.

The learning curve for coiled tubing surface equipment is well into its peak. The industry is now focusing its attention on tubing strength and tubing life. With the move toward coiled tubing drilling that began in the early 1990s, we now face learning the operational habits of bigger surface equipment. With injectors that can handle 100,000 pounds, it's becoming a whole new game. Not only is the surface equipment changing, but the steel coiled tubing itself may one day be replaced with tubing made from fiber composites. [2]

I.3.Definition :

Coil Tubing is a long metal pipe that is spooled around a large reel. The tube is continuous instead of a jointed pipe. It is normally 1 to 3.25 in (25 to 83 mm) in diameter and is used for interventions or workover operations in wellbores and sometimes as production tubing in depleted gas wells. The tubing pipe is uncurled before it is pushed into a wellbore .



FigureI.1: Coil Tubing unit

I.4. System Overview :

The coiled tubing unit is a portable, hydraulic-powered unit designed to inject and retrieve the coiled tubing workstringsafelyunder pressure to performwell maintenance and remedial services. This isaccomplished by a continuouscoil of pipe that range in sizes of 1, 1 1/4, 1 1/2, 1 3/4, 2, 2 3/8, 2 7/8, and 3 1/2 in. and largerspooled on a hydraulicallydrivenreel.

The system, adaptable to either land or offshore applications, isdesignedsothat components canbetaken off the trailer and placed on a barge for water work.

Tubing Size Range	
80K/100K CTUs	1.50 to 3.50 inch
60K CTUs	1.25 to 2.375 inch
30K Split Bodyload	1.25 to 1.75 inch
15K Single Bodyload	1.0 to 1.50 inch

Table I.1 : Tubing Size

I.5. Coiled Tubing applications :

I.5.1.Pumping applications :

- Starting a wellwithnitrogen,
- Neutralization of a well,
- Removal of sand or sediments,

- Removal of hydraulic deposits at high pressure (kerosene, salt ... etc.),
- Stimulation treatments (production column, matrix treatment by: acid, reformat, treated water, xylene)
- Hydraulic fracturing,
- Cement squeeze including other treatments for zone isolation (with sand, or polymer),
- Insulation of zones (to control production),
- Cutting of pipes with fluid.

I.5.2. Mechanical applications :

- ✓ Installation of mechanical stoppers,
- ✓ Repêchage,
- ✓ Perforation,
- ✓ Logging,
- ✓ Mechanical removal of deposits,
- ✓ Mechanical cutting of tubing .

I.5.3. Drilling applications for the unit coiled tubing :

- Drilling in Balanced or Underbalanced drilling mode,
- Deepening of vertical wells,
- Re-entry,
- Realisation of a multi-drain well from the original hole.

I.6. Advantages of Coiled Tubing :

Coiled tubing offers the following advantages :

- Efficiency .
- Self-Contained unit, requires no rig .
- Saves time and money--do not have to kill well .
- Can continuously pump fluids into well while moving pipe .
- Land or offshore system designs .
- No workover rig required when using coiled tubing .
- Reduced potential damage to formation .
- Can be and is typically used on live wells (no kill fluids introduced into well) .
- Act as tool transport medium for deviated and horizontal wells .

- Performance .
- Computer prepares to optimize job design .
- Fast .
- Tubing Management.
- Advance data acquisition system to monitor key job parameters on tubing management .

I.7. Disadvantages of Coiled Tubing :

- Low tensile strength.
- Easy to damage because of its thickness and flexibility.
- High load losses.
- Limitation to maximum pressure.
- Limited service life due to bending forces.
- Pressure differential should not exceed 1500 psi to prevent collapse of the Coiled Tubing.
- Risk of corrosion by acidification.
- Shortage of retrieval equipment that fits smaller diameters, which causes some difficulties during instrumentation operations.
- If the drill string is stuck during the ascent, the risk of abandoning it is important, because of the low tensile strength of the tubing and the lack of rotation.

I.8. Capabilities and limitations of coiled tubing :

coiled tubing offers several unique advantages and capabilities over conventional drilling methods. It also has several disadvantages and limitations of use .

I.8.1. Coiled Tubing Capabilities :

- Drilling under pressure,
- Fast maneuvering (lowering, raising),
- Continuous circulation during the pipe's advance,
- High quality and continuous bilateral telemetry between surface and downhole,
- Ability to penetrate through slim holes,
- Smaller location size,
- More secure working area.

I.8.2. Limitation of use of coiled tubing :

- No additional rotation,
- Limited drafting capacity,
- Small diameters,
- Low circulation (in case of small inner diameter of the production case),
- Short pipe life,
- Cost can be high.

I.9. Characteristics of coiled tubing :**I.9.1. Materials for the manufacture of tubing :**

The materials used to manufacture the Coiled tubing are based on very high performance steel, are rigorously controlled and have a better resistance to corrosion and hydrogen sulfide.

Virtually all CT in use today begins as large coils of low-alloy carbon-steel sheet. The coils can be up to 55 in. wide and weigh over 24 tons. The length of sheet in each coil depends upon the sheet thickness and ranges from 3500 ft for 0.087 in. gauge to 1000 ft for 0.250 in. gauge. The first step in tube making is to slice flat strips from the coil of sheet using a slitting machine (**Figure I.3**). A specialist company usually performs this operation and ships the coil of strip to the CT mill for further processing (**Figure I.2**). The sheet's thickness sets the CT wall thickness and the strip's width determines the OD of the finished CT.

In some cases the gauge of the sheet material is tapered over a portion of its length, as is shown in (**Figure I.4**). This variation in thickness is used by Quality Tubing to produce CT with a wall thickness that varies along its length, known as "True-Taper™".

The CT manufacturer splices strips with similar properties together using bias welds to form a single continuous strip the length of the desired CT string. This strip is stored on an accumulator called a "Big Wheel", (**Figure I.5**) Joining strips of different thickness or using strips with a continually changing thickness yields a tapered string. The CT mill forms the flat strip into a continuous tube and welds the edges together with a continuous longitudinal seam.

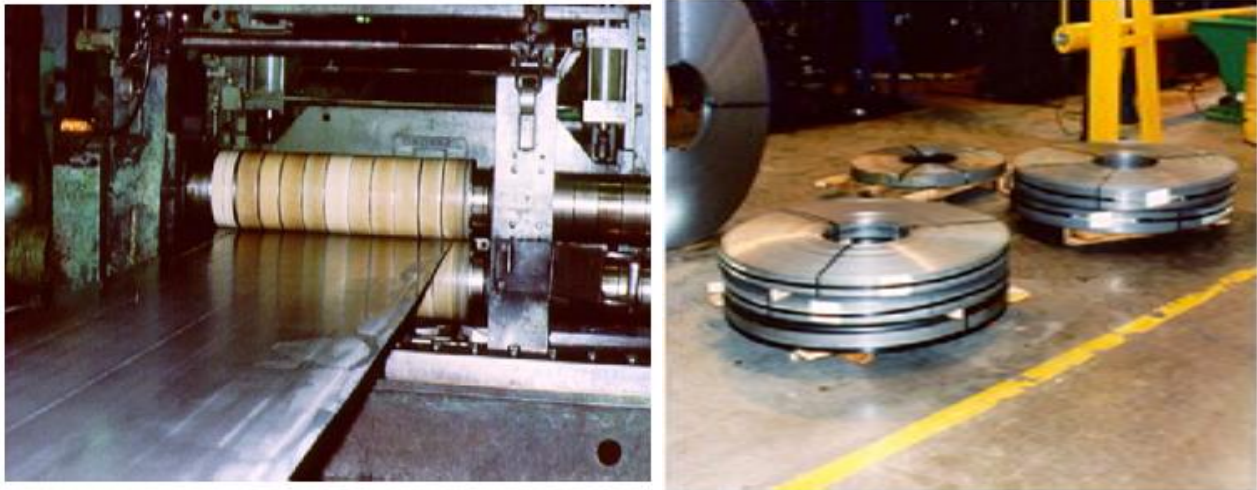


Figure I.2: Slitting Steel Sheet for Strip Figure I.3 : Rolls of Steel Strips

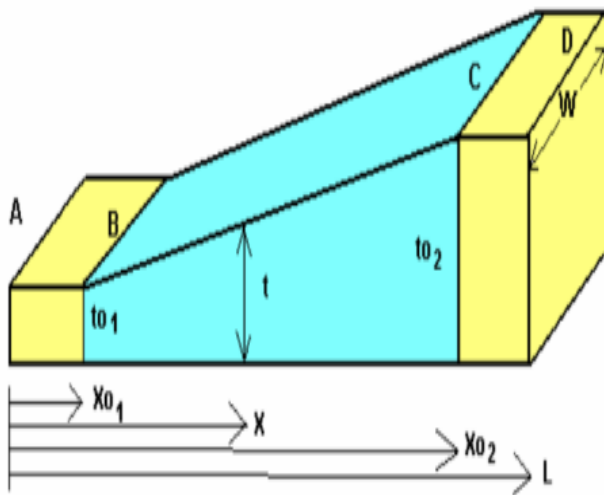


Figure I.4 : True-Taper™ Figure I.5 : “Big Wheel” of Flat Strip

I.9.2. Forces applied to Coiled Tubing :

The forces applied to the Coiled Tubing during its service life are :

- Crushing stresses due to external pressure.
- Bursting stresses due to internal pressure.
- Tensile stresses that can cause elongation or rupture of tubing.
- Compressive stresses in deviated wells that can cause buckling.
- Cyclic bending stresses between the reel and the sprue head.

The combination of all the forces reduces the life span of Coiled Tubing.

I.9.3. The critical deformation moment of Tubing during the maneuver :

- At the beginning of the unwinding and winding of the tubing on the drum when it goes from the curved state to the straight state and vice versa.

- At the moment of passage on the gooseneck when the tubing passes from the straight state to the curved state and vice versa.
- At the moment of passage from the gooseneck to the injection head when the tubing passes from the curved state to the bending state to the straight state and vice versa.

A fatigue cycle for a Coiled Tubing is defined as the set of sequences, from from unwinding and rewinding on the drum, to lowering and rewinding on the goose neck. and this reduces the tensile strength by about 5 to 10% of its yield strength. of its elasticity limit.

The service life of a Coiled Tubing is generally considered to bear around 80 cycles, without taking into account the effects of pressure without taking into account the effects of pressure, acidification and weight.

I.10. Conclusion :

In the end it was discovered that there are more benefits than disadvantages in using coiled tubing services.

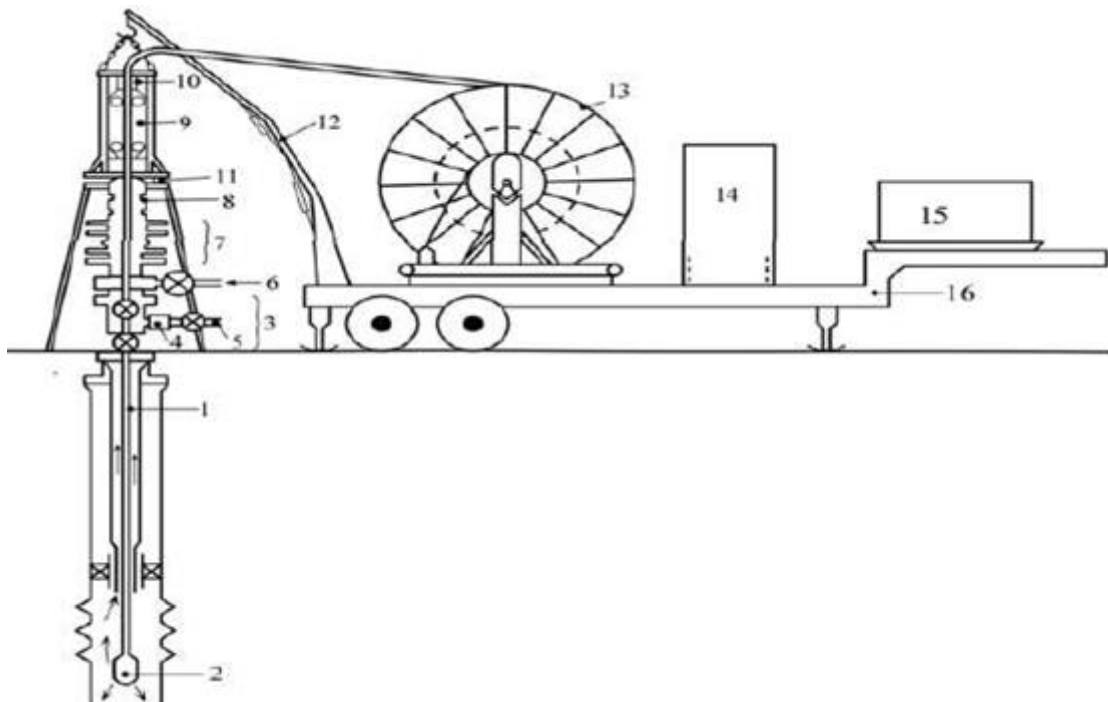
ChapterII:

Operating principle of the Coiled Tubing

ChapterII: Operating principle of the Coiled Tubing**II.1.Introduction :**

The Coiled tubing is a unit consisting of all the equipment necessary for the continuous execution of tubing length operations in the field. The unit consists of two main parts :

- Surface equipment.
- The bottom tools .



FigureII.1 : coiled tubing equipment

1. Coiled tubing
2. Circulation tool
3. Wellhead
4. Production nozzle
5. Production line
6. Manifold outlet
7. Bop
8. Stripper
9. Injector
10. Rectifier
11. Weight indicator
12. Crane
13. Reel
14. Control cabin
15. Power pack
16. Trailer

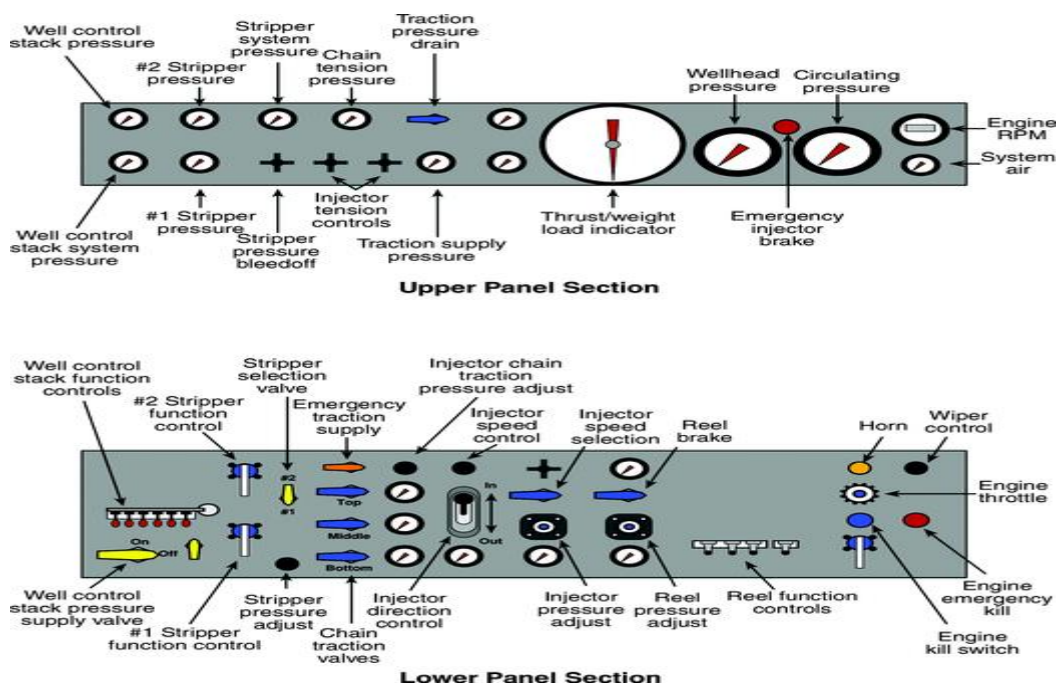
II.2.Surface equipment :

II.2.1Control cabin :

The design of the CT unit control booth may vary among manufacturers, but normally all controls are located on a remote console panel. A schematic of a typical CT unit control panel is shown in **Figure II.3**. The console assembly is complete with all the controls and gauges needed to operate and monitor all the components used and can be skid-mounted for offshore use or permanently mounted as for land-based units. The skid-mounted console can be placed wherever the operator wishes at the well site. The reel and injector motors are activated from the control panel by valves that determine the direction of casing movement and operating speed. Also on the console are the control systems that regulate the pressure of the drive string, stripper assembly and various well control components...

The operator must have all the necessary controls in front of him to operate, control and monitor the following parameters :

- Circulation pressure
- Wellhead pressure
- Casing weight
- Tool depth
- Operating speed
- Circulation flow rate
- Pumped volume Winch
- Injection head
- BOP
- Stripper



FigureII.2 : Simplified layout of a console control panel**FigureII.3 : Control cabin**

II.2.2. Power unit :

The hydraulic power required to operate the various components and equipment of the Thehydraulic power required to operate the various components and surface equipment of the coiled tubing unit (drum, injection head, BOP, The power unit (**Figure II.4**)isnormallyequippedwith an automatic emergency stop system in case of significanttemperature and oil pressure variations. The hydraulicpumpssupply six circuits used to control the variousfunctions of the coiled tubing unit. functions of the coiled tubing unit whichare :[1]

- the first circuit with a maximum working pressure of 3000 psi issupplied by twopumps (60 and 30 g/min)pumps (60 and 30 g/mn) and drives the injection head.
- the second circuit with a maximum working pressure of 2000 psi drives the winch drum.
- The third circuit, with a maximum working pressure of 2,500 psi, drives the devicethat guides the winding and unwinding of the tubing.
- the fourth circuit is the BOPs circuit whichallows the accumulators to berecharged to a maximum pressure of 3000 psi.
- The fifth circuit iscomposed of storagecylinderspressurized to 2000 psi which, with the help of regulators, performs the followingfunctions and organsfunctions and components by means of the regulators:
 - tensioning the innerchain of the injection head at a pressure of 1500 psi.
 - the tension of the outerchain of the injection head at a pressure of 400 psi.
 - the speed of the injection head at a pressure of 600 psi.
 - the forward/reverse rotation of the injection head at a pressure of 600 psi

- cab position adjustment at 600 psi.
 - Hydraulic winch drumbraking system at 350 psi.
 - the coiled tubing synchronization system on the drum at a pressure of 2000 psi.
 - The system for adjusting the high or low position of the injector at a pressure of 600 psi.
- the sixth circuit used to supplyauxiliaryauxiliaryequipment of the coiled tubing unit



FigureII.4 : Power unit

II.2.3. Winch drum :

The drum is a device that allows the coiled tubing to be unwound, rewound and stored as a whole. In order to reduce the severe bending forces that the coiled tubing undergoes during its winding and unwinding, the drum must have a sufficiently large diameter, the storage capacity can be between 5000 - 22000 ft .

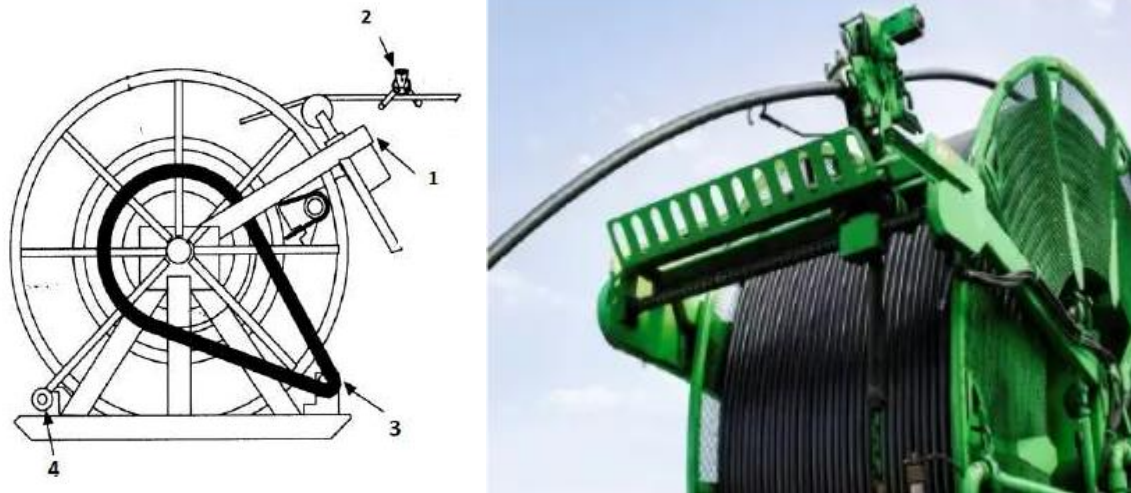


Figure II.5: Simplified layout Figure II.6 : Winch drum

Showing Winch drum

1. Lubrication system
2. Weight indicator
3. Drive motor
4. Braking system

II.2.4. Injection head :

The injection head(Figure II.7) is a main component of the coiled tubing unit, used to operate with the help of two hydraulic motors that drive two continuous chains on which are mounted gripping elements that push or pull the coiled tubing into the well during operations.[4]

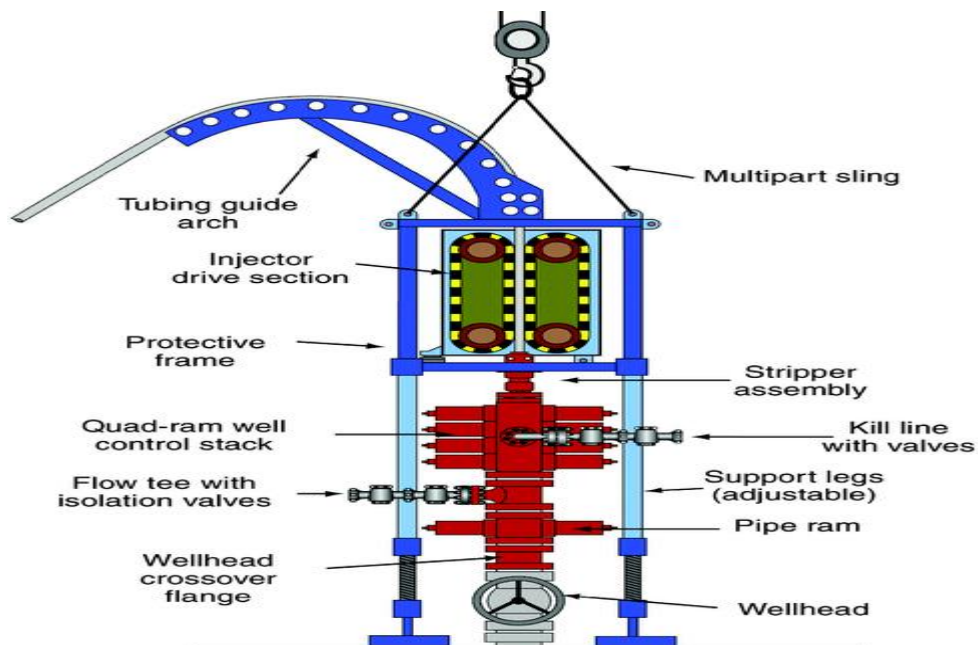


Figure II.7 : Injection head assembly

Both hydraulic motors are driven by the same pressure source to avoid phase shift between the two chains.

The traction capacity of the injection head is a function of :

- the size of the injection head.
- the working pressure chosen by the operator from the power unit .
- the chosen speed which is normally around 125 ft /mn (low speed) and 250 ft/mn (high speed) .

The seizing force is obtained by actuating three hydraulic pistons through the inner part of the two chains of the injection head (Inside tension cylinders). This force must be sufficient to prevent slipping and crushing of the tubing. The outer piston keeps the two chains under tension.

The entire injection head is mounted on a substructure equipped with a tubing weight cell connected by a hydraulic hose to the weight indicator in the operator's cabin.

II.2.4.1. Gooseneck :

The role of swan neck, to guide and receive the tubing after its unwinding from the drum, connected to the injection head with a very sophisticated system (**Figure II.8**).

To obtain the desired radius of the gooseneck, a number of bearings are placed in its curvature frame with a coiled tubing alignment system.

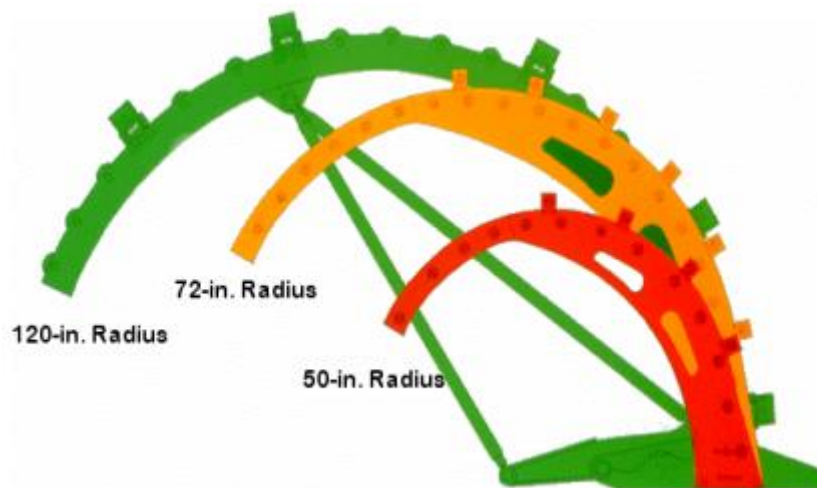


Figure II.8 : Gooseneck

II.2.4.2. Drive Chains and Tensioners :

The drive system consists of two hydraulic motors typically connected and synchronized by a control system. The direction and speed of rotation of these motors is controlled by a 4-position hydraulic control valve located at the power pack.



FigureII.9 : Chains and Tensioners

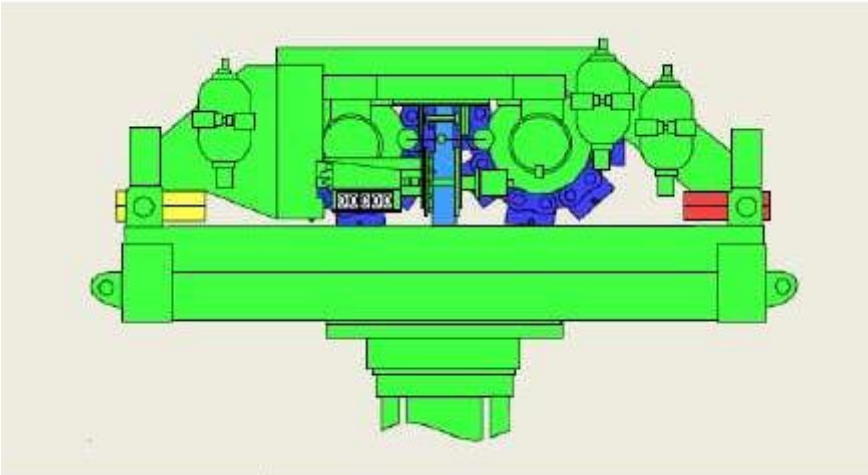
II.2.4.3. Chain component :



FigureII.10: Chain component

- 1. Axes de liaison
- 2. Gripper
- 3. Chaîne à rouleaux
- 4. Goupilles fendues

II.2.4.4. Weightindicator :



FigureII.11 : Weightindicator [1]

II.2.5. Packer (stripper) :

The stripper (**Figure II.12**)is a sealingelementwhichisinstalledunder the injection headvery close to the grippingelements of the injection headchain in order to prevent the coiledtubingfrombucklingduring the operation.

The stripper is the primarybarrierwhen the coiled tubing is in the well, itensures a perfectsealaround the coiled tubing like the gland in cableoperations.

There are three types of stripper on the market :

- the conventional stripper
- the conventional stripper
- radial stripper

The operating principle of all types of strippers is the same, itconsists of hydraulicallymoving a piston to directly or indirectlycompress a seal, whichhydraulically move a piston to directly or indirectlycompress a seal, which in turnsealsaround the coiled tubing.[4]



FigureII.12: stripper

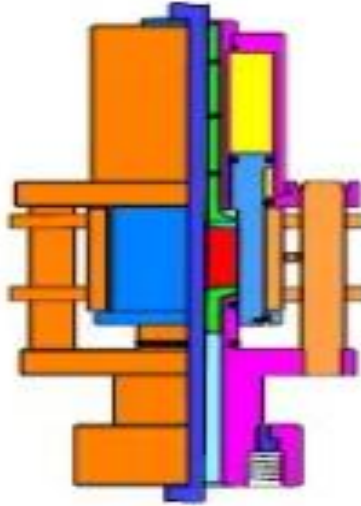
II.2.5.1. The conventional stripper :

In the conventionalstripper (**Figure II.13**) the hydraulic pressure appliedpushes the piston upwardswhich in turn moves the lower fur to compress the packeragainst the upper fur.

The pressure at the top of the well tends to keep the stripper closedduring the intervention operation, which

The wellhead pressure tends to keep the stripper closedduring the intervention operation, thusreducing the hydraulic pressure in the lowerchamber of the stripper.

The upper and lower sleeves help guide and center the tubing in the packer seal. A ring mounted between the upper sleeve and the seal prevents the seal from being forced between the upper sleeve and the seal. A ring mounted between the upper sleeve and the seal prevents the seal from being forced between the sleeve and the Coiled Tubing.



FigureII.13 : conventional stripper

II.2.5.2. The lateral stripper :

The operating mechanism of the sidedoor stripper (**Figure II.14**) is reversed compared to the conventional stripper.

In the sidedoor stripper system, the hydraulic pressure pushes the piston down, which in turn moves the upper liner, which presses the packer around the tubing against the lower liner.

The hydraulic pressure applied to the piston must be greater than that of the wellhead and must be maintained during the entire intervention operation.

The table below shows the characteristics for each type of stripper:

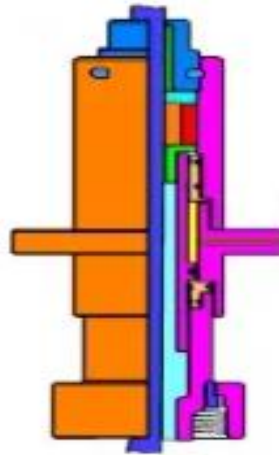


Figure II.14 : lateral stripper [4]

II.2.5.3 Radial stripper :

The Radial Stripper (**Figure II.15**) is a stripper with jaws designed specifically for Coiled Tubing stripping. It was developed to overcome the problems encountered during the use of conventional strippers (single or double).

The radial stripper has a reduced height, ease and simplicity of change of elastomers compared to the conventional stripper.

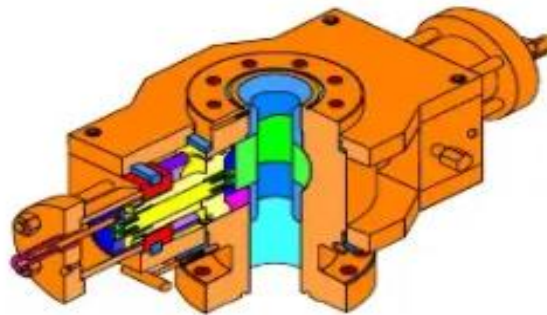
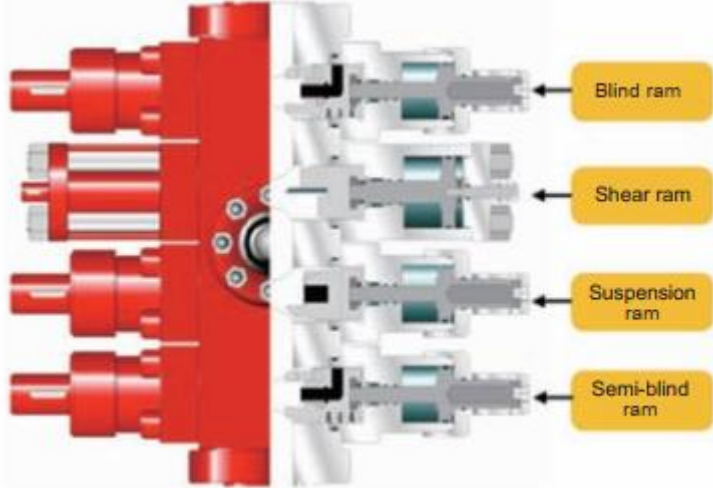


Figure II.15 : Radial stripper

II.2.6. Blowout Prevention System (BOP) :

The blowout prevention system mainly includes BOP, blowout box and lubricator. As the well control equipment of oil and gas wells, the blowout prevention system functions mainly in sealing the pressure in wells and preventing blowout accidents etc. during field operations with the coiled tubing unit.

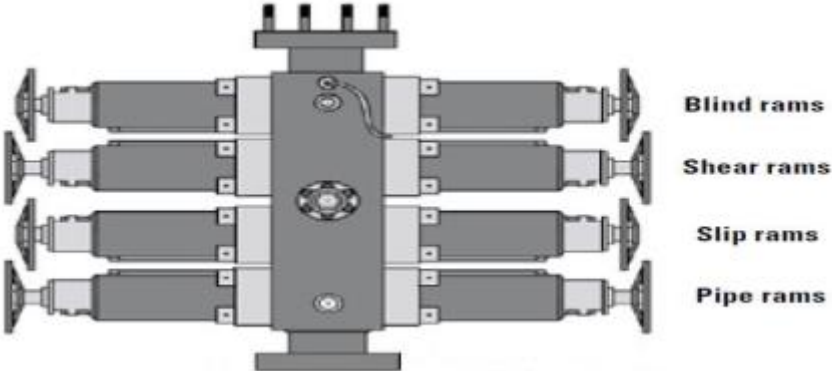


FigureII.16 : BOP [3]

II.2.6.1 Quadruple BOP :

This type of standard stacking is the most responsive of the BOPs used in Coiled Tubing, it is a solid block composed of four rams arranged (Figure II.17) from top to bottom as follows .

- A blind rams plug: Used only to seal on an empty hole.
- A shear rams plug: used to cut Coiled Tubing / Coiled Tubing with logging cable inside without sealing.
- A slip rams packer: used to suspend the tubing in the well without sealing.
- A pipe rams plug : used to obtain a positive seal against the tubing .



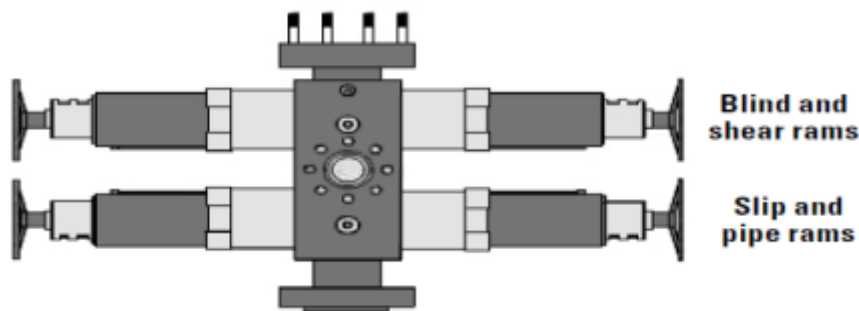
FigureII.17 : Quadruple BOP

II.2.6.2. Combinaison BOP :

The BOP COMBINE (**Figure II.18**)is a double shutterwhichfulfils the samefunctions as the BOP QUAD but withonlytwo rams, itiscomposed of :

- A Blind/Shear rams top plug, used to cut the tubing and seal on an emptywheel.
- A lower pipe/slip rams plug, used for hanging and sealing on the tubing.

Each valve isequippedwith a pressure equalization valve. A kill line inletlocatedbetween the thetwoobturatorwhichallows to pumpinside the tubing if necessary.



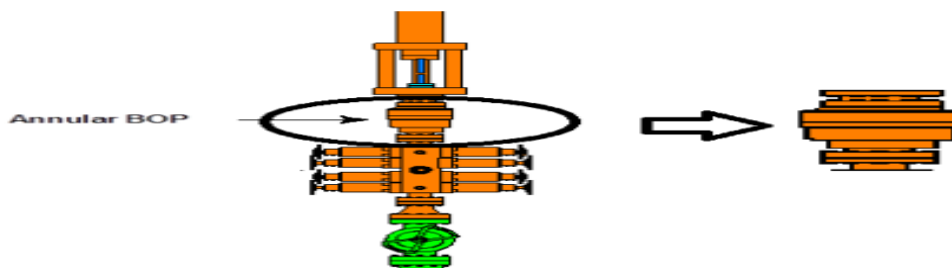
FigureII.18 : Combinaison BOP

II.2.6.3Annular BOP :

The Annular BOP isused more frequently in specialoperations at the Coiled Tubing, for example the assembly of very long tool strings thatrequire the use of a deployment system. The main purpose of using an annular stopper in a CoiledTubing stackis to be able to close stackis to be able to close tightly on differentdiameters of Coiled Tubing and tooling.

Its position in the stackdepends on the nature of the work to bedone. above Quad, below the deployment system, the ring shuttercanbeused as a back up as a back up for the stripper if necessary.

The characteristics of the annularshutter must besimilar to those of the clamshellshutterswith the with the additionalpossibility of closing on an empty ho

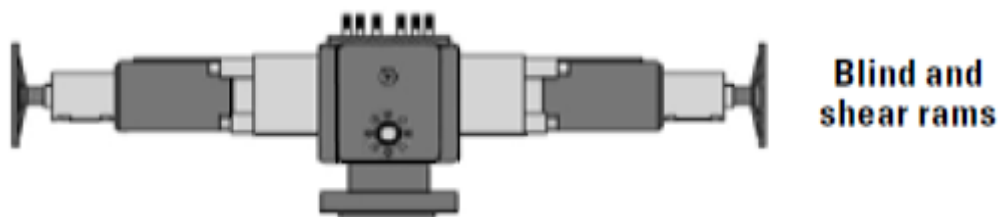


FigureII.19 : Annular BOP

II.2.6.4 Shutters (shear/seal) :

In some countries where safety regulations are very strict, an additional shear/seal rams (**Figure II.20**) must be installed between the production head and the BOP assembly, and is used as a tertiary barrier if necessary.

This type of valve requires a large volume of hydraulic fluid, which is why an independent hydraulic unit (kooomey) is required. The working pressure of the kooomey unit is usually between 1500 and 3000 psi .



FigureII.20 : Shutters (shear/seal)

II.2.7. Deployment system :

In Coiled Tubing operations, the distance between the production wellhead and the stripper determines the maximum length of the tool string. If this maximum distance is exceeded, it becomes necessary to use a control barrier which can be the DHSV or the deployment system.

In general, there are several types of deployment systems on the market (**Figure II.21/ II.22**) which have the same operating principle as the multi-ram BOP .

The stacking can be composed of :

- one shear/seal rams on top and one pipe rams on bottom.
- a tubing /slip rams plug at the top and pipe rams to guide the tubing at the bottom.

The advantage of using the deployment system under the QUAD or the COMBI is to be able to assemble the different sections of a relatively long toolpath when lowering and to assemble them when raising of a relatively long toolpath in complete safety. [4]

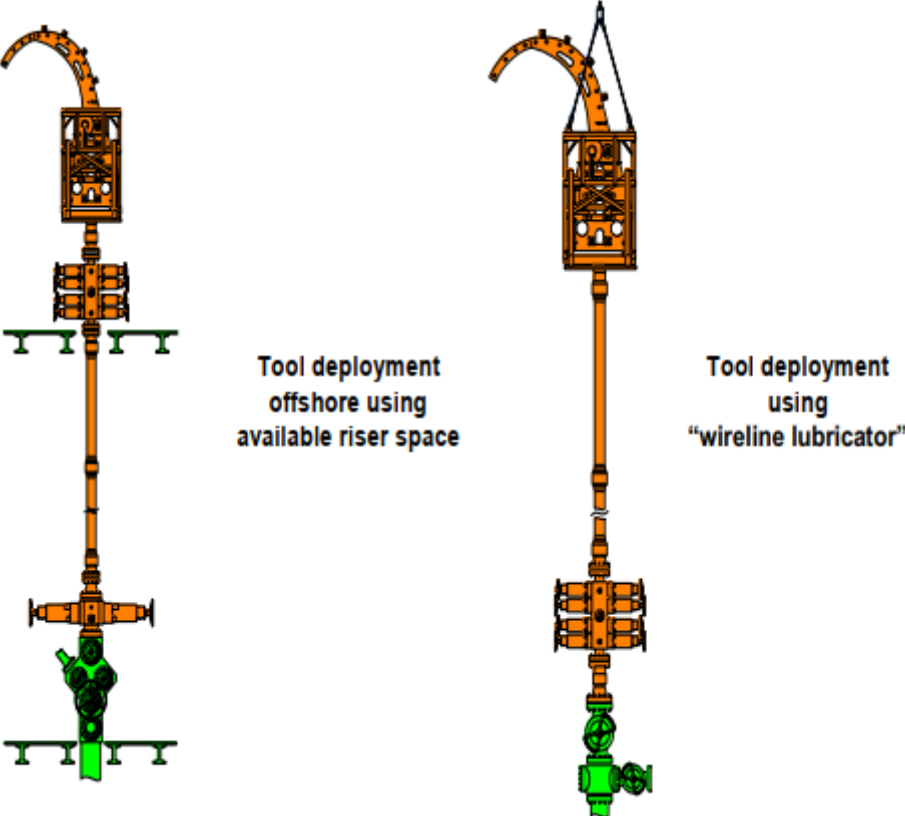


Figure II.21 : offshore deployment

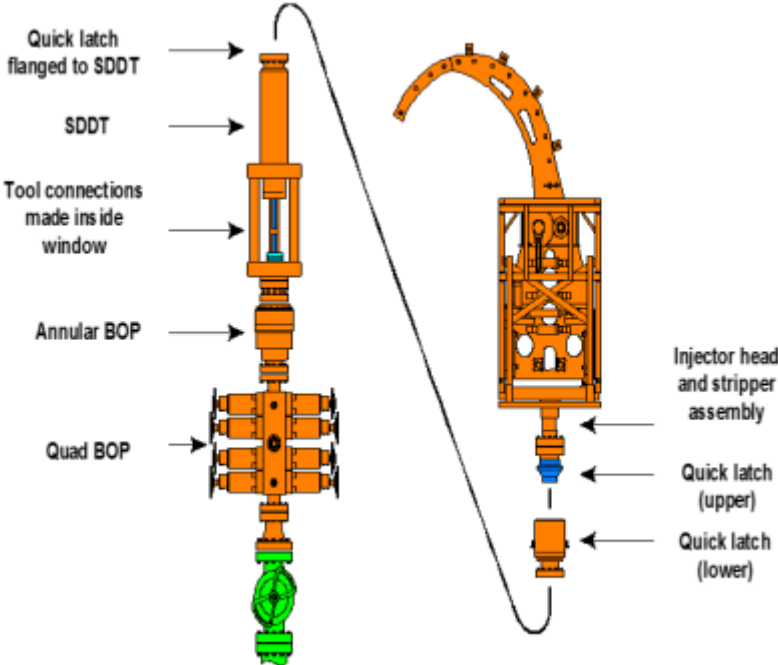


Figure II.22 : onshore deployment

II.3. The bottom tools :

It is a set of parts that constitutes the main element of coiled tubing (the train or the probe of coiled tubing).

The coiled tubing train is valid for the different coiled tubing operations, such as cleaning, re-drilling, stimulation, acidification ... etc, attached to the end of tubing. The main elements are:

II.3.1. Fitting (connector) :

Coiled Tubing fittings(**Figure II.23**) are used to couple various downhole tools to the end of the Coiled Tubing. There is a wide variety of fitting types and sizes on the market. There are three types of fittings used for coiled tubing:

Bite fittings, screw/hole fittings and internal fittings.

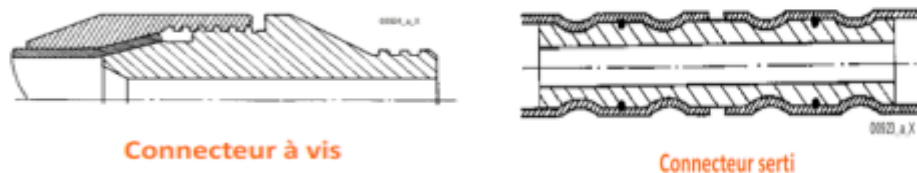


Figure II.23 : types des connecteurs

II.3.2. Check valve :

The probability of reverse circulation with Coiled Tubing is very low, so the use of check valves in the use of check valves (**Figure II.23**) in the Coiled Tubing train becomes necessary .

Generally the check valve is placed at the top of the BHA, immediately below the load bars.

Check valves can be ball or flap valves and are considered the primary barrier during the intervention at the Coiled Tubing.

If the check valve fails, the Coiled Tubing must be reassembled with circulation to prevent well fluid from passing into the Coiled Tubing.

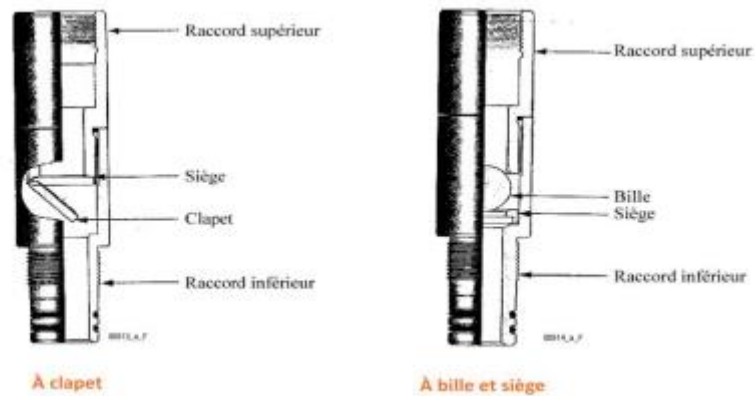


Figure II.24 : check valve

II.3.3. Hydraulic disconnecter :

Hydraulic disconnecter (Figure II.24) is a shear lowered with the tool train to release the Coiled tubing in case of jamming, the principle of use of the Boss is to pump a ball inside the Coiled tubing and continue to rise in pressure until shearing the pins of the disconnectors and release the Coiled Tubing. [4]

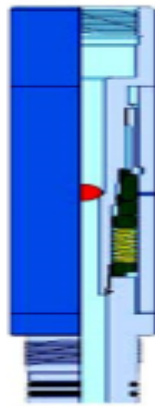


Figure II.25 : disconnecter

II.3.4. Centerers :

The centering devices are securely mounted in the coiled tubing tool set to keep the tools or the the tools or the tip away from the walls of the tubing material.

- Elastic blade centering device :

Elasticblade centering machines usually have three flexible curved blades. The elasticity of the blades allows for effective centering within a certain range of inside diameter.

➤ **Rigid centering device :**

Rigid centering devices usually have three or four fins mounted on a central sleeve. The outside diameter of these fins is slightly smaller than the smallest inside diameter encountered in the diameters encountered in the packing through which it is to be lowered.

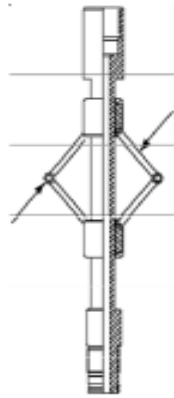


Figure II.26 : Centerers

II.3.5. The load bars :

Used to increase the train size (length), and center the assembly in the empty area between packer and between packer and liner.

II.3.6. Patella :

The ball-and-socket joint (**Figure II.26**) minimizes the effects of coiled tubing bends and gives the BHA the flexibility to centralize heavy components.



FigureII.27:Patella

II.3.7. The tool :

There are several types of tools(**Figure II.27**)used, depending on the operationwemake the choice (of tool). The cuttingtool, the cleaningtool, and fishing ... etc.[4]



FigureII.28 : differenttools

II.4. Conclusion :

We note that the coiled tubing group consists of manyequipment on the surface as well as the bottom, whichmakesit more advantageous, coordinated and efficient than the rest of the groups, and thishelps the drillingprocess and gives a distinctive result.

III.1 INTRODUCTION :

Teg-37 was drilled and completed by KCAD T220 on 10th November 2012, The well was put on production on the 5th April 2013, and after 15 days flowing the well started to be loaded with production fluid (heavy fluid) and caused the dead of the well , The static Gradient surveys analysis indicated that the top of this heavy fluid is at 2500 m, and this fluid has a pressure gradient of 0.4 psi/ft, above this fluid we have a dry gas with SG = 0.628 and 9.2 mol % CO₂.

The 4-1/2" Slotted liner in this well is not installed properly deep in the well and is suspended completely inside the 7" Casing, as you can see below Schematic, This was due to a problems encountered during the completion of the well.

Mud losses were observed during the drilling of the 6" Hole, Estimated quantity of OBM lost is as below.

A fish was left inside the 4-1/2" Slotted line during the completion of the well, dimensions of the fish are mentioned below .

III.2. Objectives :

Teg-37 is being drilled to be completed as vertical gas well located in the In Salah field. A clean up operation is planned to be performed on this well, therefore JV-Gas has requested from Halliburton to unload the well.

The well is new drilled Gas well and was put on production on the 5th April 2013, But just after 15 days the well started to be loaded with production fluid (heavy fluid) and caused the dead of the well , The static gradient surveys analysis indicated that the top of this heavy fluid is at 2500 m, and this fluid has a pressure gradient of 0.4 psi/ft, above this fluid we have a dry gas with SG= 0.628.

This proposal describes the procedure, material and equipment required to perform this job.

To kickoff the well with N₂ and flow it until it is clean from hydrocarbon liquid using Schlumberger Well Test Unit and HES Coiled tubing unit, The aim of the displacement is to recover all liquids from the well and draw the well to lowest possible FWHP and get measurement of the Condensate Gas Ratio (CGR) in the end of the clean up, All clean up fluids will be taken to the flare pit and burned / evaporated .

III.3. Program Overview :

RU with Slick-line and drift tubing and Tag HUD with appropriate drift size, use 3.35” fluted drift (1-3/4” CT will be used), then rigged down with Slick line, RU with Schlumberger Well Test equipments and Pressure test surface equipment, Coiled Tubing will then be rigged up and run in hole, and the well will be unloaded using N₂. The aim is to run the coil to inflow the well and clean up. After the well observed flowing continuously in the flare pit, pull out of the hole while circulating at low N₂ flow rate to surface, continue flowing the well until confirming the well is cleaned up from liquids.

III.4. Presentation of the krechbafield :

III.4.1 INTRODUCTION :

The Krechba deposit is located in the northern part of the In Salah region (figure III.1). The deposit was discovered in 1957 by drilling KB1 which returned counter the Tournaisian Carboniferous and Siegenian – Gedinnian reservoirs of the Lesser Devonian at a depth of 1,700 to 3,350 meters. The different drilled wells produced gas flows in all three reservoirs. This deposit constitutes, with those of Teg and Reg and, further south, those of the In Salah region (Hassi Moumen, Garet el Befinat, Gour Mahmoud and the structure of In Salah), a large gas complex operated as part of the Sonatrach – BP – Stat Oil. After treatment, the gas produced is transported to Hassi R'mel located 450 km north of Krechba

(Figure III.2). [5]

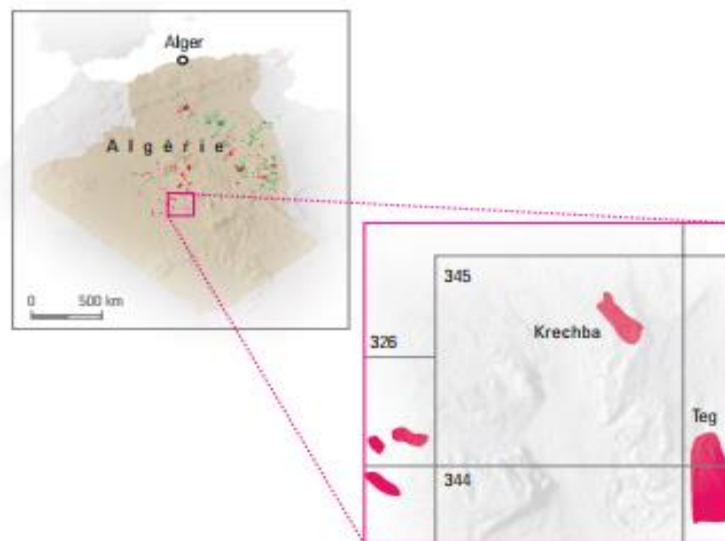


Figure III.1: Situation map of the Krechba deposit.

III.4.2. structurally of Geology :

The Krechba deposit appears to be a large anticlinal structure closed, structurally simple. The current architecture of the Krechba was modeled at the end of the Carboniferous during the "Hercynian orogeny born ". This is an anticline that developed as a result of cutbacks deep in the base. These were accompanied by a network of north-south faults intersecting, to the west of the deposit, the formations of the Ordovician and the Silurian.

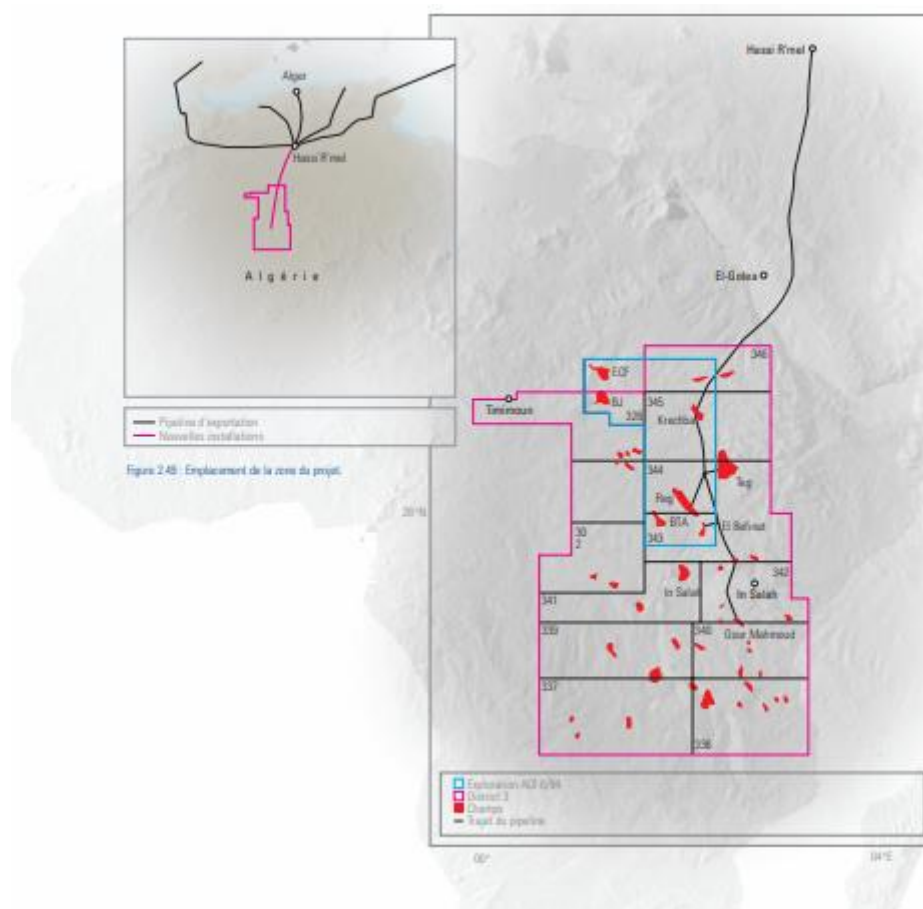


Figure III.2: Location of Project Area

The location of the paleovalley, in which the sandstones of the Tournaisien were deposited, was influenced very presumably by these flaws. The structure of Krechba underwent post-hercynians. The structural map of the Krechba deposit has been established on the basis of the interpretation of the seismic 3D carried out in 1998, the three reservoir horizons having then been mapped in detail. The interpretation shows an elongated submeridian NNO-SSE

anticline with fer-metures with steep sides (**Figure III.3**). Figure 2.51 shows the stratigraphic column as well as the nomenclature adopted in the series.

III.4.3. The Carboniferous:

Carboniferous sandstones, deposited in an environment of paleovallée, are located at a depth of 1,700 m. These sandstones are well developed (up to 24 m thick total) over a large part of the deposit, but are absent in parts of western and southern field. The Carboniferous sandstones are of good quality, with porosities up to 22% and permeabilities up to 200 mD. The body of water at the level of Carboniferous is at the level of -1 330 mss, which gives a closed area of 130 km². This body of water was confirmed by pressure measurements and recorded tests.

III.4.4. The Devonian :

The Devonian reservoirs are located at a depth between 2850 and 3350 m; they come under the form of alternating sandstone levels separated by clay levels. These sandstones are of "little marine deep" to "marginal sailor". Gedinnian sandstones (D30 to D10) have a significant lateral extension and are of medium quality, with porosities up to 15% and permeabilities reaching 150 mD. The sandstone from the Siegenien (D40) are of poorer quality due to diagenesis; porosities are generally less than 10%. In the Devonian levels (D40, D30 and D20), the trapping mechanism is complex. The area of the roof closure of the D40 is 100 km² with a structural closure of 65 m. However, for the two tanks D40 and D30-20, the gas column interpreted from the logs exceeds the height of the structural closure. For D40, the trapping mechanism is probably mixed, structural or stratigraphic / diagenetic. Gas / water contact has been confirmed at -2,420 mss by tests and pressure measurements. [6]

III.4.5. Well testing and reservoir fluids :

The results of the tests carried out on the Carboniferous and Lower Devonian look like this:

- Tank C10.2
- The DSTs of existing wells, despite their short lifetimes, show variation in productivity from one well to another. This variation in flow rate is a function of reservoir qualities and is an indicator of its heterogeneity. [7]

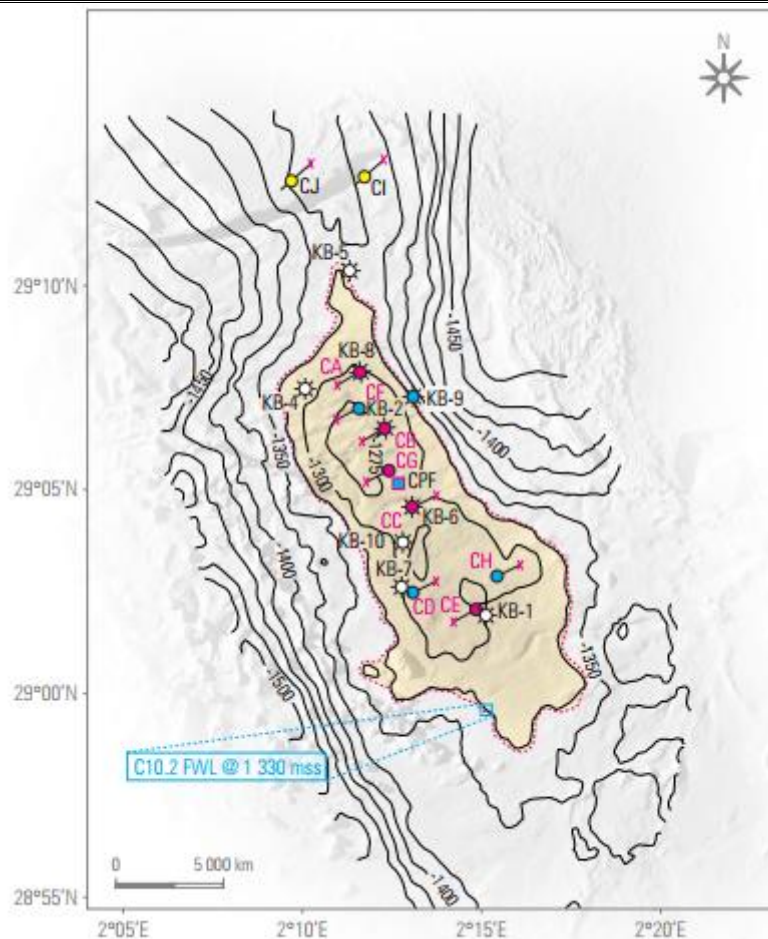


Figure III.3 : Structure of the Krechba deposit.

The results indicate maximum production in wells not damaged, which varies from 300,000 m³ / d on the sides to 700,000 m³ / d in the center of the structure. Analysis of the fluids collected indicates a variation in the gas composition, with a maximum condensate content of 11.2 m³ / million m³ obtained on the KB-9z well. The maximum condensate flow obtained has summer of 1.4 m³ / d.

D30 tank The test results show a variation in the production rate. The Flow rates obtained from the wells in the north of the field were greater.

Some wells provided appreciable flows. The flow variation is directly linked to the qualities of the reservoir and indicates its heterogeneity. The production of water observed during certain tests confirms the complexity of the body of water in this reservoir. We will note other share the high concentration of CO₂ (9%) obtained on the effluent of the KB10 well.

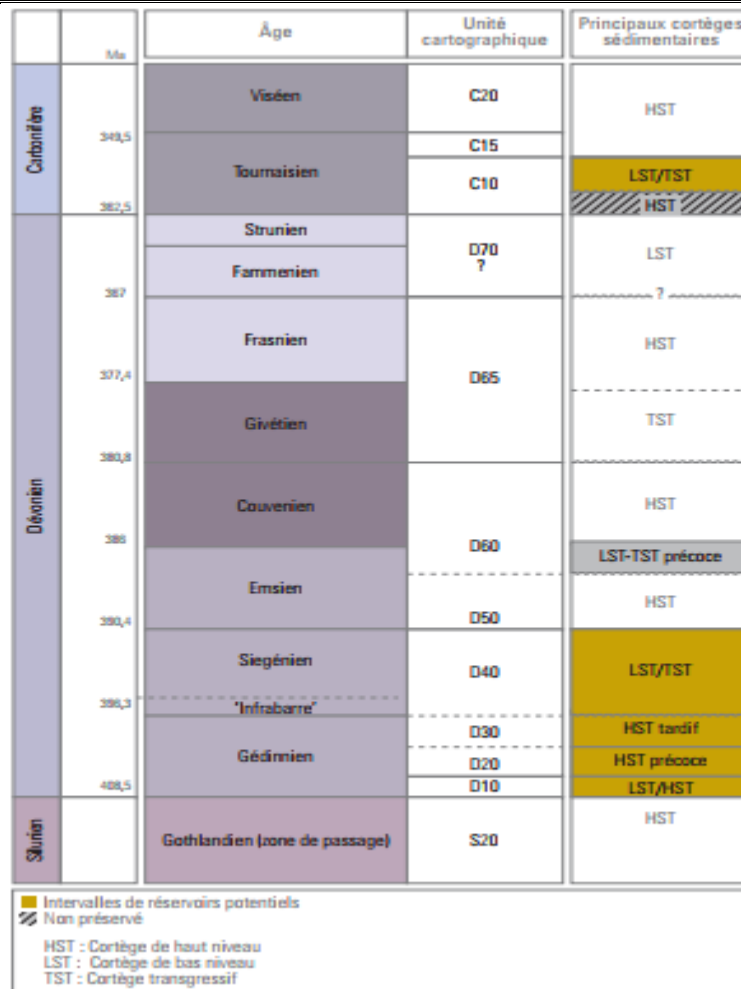


Figure III.4 : Stratigraphic column

III.4.6. Well Data: [7]

Production Rate: 50 mmscfd @ 56 barg (During last clean up)

Max Deviation: Vertical Well.

Min ID: 3.725" RN Nipple @ 2592.5 m MDbrt

Last DownholeOps: Drift HUD and performed SBHPS (Static bottom hole pressure surveys) On 27-April-2013, Tagged HUD at 2757m(WL)

Target Reservoir: D40 Lower sand

kh 4229 md-ft

Reservoir pressure from initial build up 1987 psi at 2969 mtvd

- ◆ ***Fish dimensions:*** The fish was left during running the 4-1/2" Liner, and was tagged during Slick line job with 3.35" fluted drift at 2757 m (WL). Lost tools string composed by.
 - *Flapper Valve shifting tools (0.67 m)*
 - *2-7/8" EU Pin / Pin XO (0.27 m)*
 - *No-Go Sub (0.35 m)*
 - *2-7/8" string shoe (3 m)*

III.5. Service Companies Responsibilities :

III.5.1. Responsibilities of Schlumberger Well Test crew :

- Function test methanol injection pumps at the choke manifold prior to start of test.
- Tie cable/clamps will be used in all upstream lines. Swamp weight shall be used on the flare lines.
- Ensure that gas detection equipments will be on site, and functioning.
- Function test the ESD, from all shut down points check the set pilots low and high
- All pressure testing will be with appropriate permits, and test area barricaded
- The material safety data sheets for all chemicals stored on-site during testing operations will be made available.
- Thickness testing of the flow lines should be conducted every 1-2 hrs, during the clean up Periods, If significant amounts of solids are lifted, then the thickness measurements of the pipes should be more frequent (less than 1 - 2 hours), paying particular attention when there is an increase in flow rate and when the slotted liner is being jet blasted
- Withdraw all hot work permits before start of the test.

III.5.2. Responsibilities of Halliburton Coiled tubing crew

- If only one stripper is supplied with the CT spread there must be two pipe rams. This is to comply with two barrier policy. If two strippers are used then the upper stripper is the one which should be used when carrying out the CT operation. When shear seals are employed all connections to the tree or wellhead must be flanged and double valve isolated, thereby excluding elastomers from connections beneath these BOP's. Ref: BP DWOP (BPA-D-001- Section 23. Coiled Tubing Operations).
- BOP must be flanged to X-mass tree.
- Confirm crane is capable to lift the injector head

III.6. TECHNICAL INFO AND WELLBORES SCHEMATIC :

III.6.1. Customer Wellbores schematic :

Table III.1 : completion Schematic

FINAL COMPLETION SCHEMATIC				FIELD: TEGUENTOURINE				WELL NUMBER: Teg-37				
WELLDATA				CASING DATA								
Well Type:	7x5 Prod	Endofstring:	2603m	Original RTE:	9.15	Size(n.)	Weight	Grade	Thread	MD(m)	TVD(m)	
Original Drilling Rig:	KCADT 220	Annulus Fluid:	NaCl Brine	New RTE:	N/A	30	310ppf	X56	Welded	5	5	
New Drilling Rig:	N/A	Annulus Fluid:	1.03	Minimum string ID:	3.502in.	18%	87.5&100.5ppf	K55	Buttress	77	77	
First Completed:	10-Nov-12	Completion Fluid:	NaCl Brine	Well ID:	2999m DDbt	13%	69ppf	K55	Buttress	908	908	
Workover Number:	N/A	Completion Fluid Wt:	1.03	Max DL 5'(30m):	0.9	10% (w/ 9%)	55.5ppf	L80	Vam Top	91	91	
Workover Date:	N/A					9%	47ppf	L80	Vam Top	1865	1865	
WELLHEAD DATA				LINER DATA								
	SUPPLIER	TYPE	RATING	TOP CONNECTION	Size(n.)	Weight	Grade	Thread	MD(MDD)	TVD(m)		
XMASTREE CAP	Cameron	6.3/8" FLS	5M	9.1/2" OTIS Quick Union	7" Liner	1794	L80	Vam Top	2868	2868		
XMASTREE	Cameron	6.3/8" FLS	5M	7.1/16" API Studded	4 1/2" Slotted Liner	2600.8	L80	Vam Top	2793.8	2794		
2STAGE WELLS HEAD	Cameron	S3MC	5M	135/8" Flange Lock								
TUBING HANGER	Cameron	135/8"	5M									
ADDITIONAL COMPLETION INFORMATION				RESERVOIR ZONES:								
KCADRTE to hang off point (m):				9.39	PACKER:	0.90	D40	2937.5m DDbt	2937.5m DDbt	144°C	2195 Psia	
				0.47	Top of Packer to mid element (mBRT):	2557.43						
					Mid Packer to mid element (mBRT):	2572.5						
					Nearest 17" casing couplings (mBRT):	21.3						
					Gap from 7x5" Crossover to 9-5/8" 7" TOL							
COMMENTS/NOTES:				CONTROLS:								
X-mas Tree: S/N: 112183945004/P/N: 2205085-01				Gap from end of production string to the top liner PBR				3.90	TRSV: 5" Inflow Controlled Control with 1/4" Swivel offsetting.			
KVY: S/N: 112184092-004/P/N: 2230971-01				Maximum circulation before bottom nipple				0	5" Cannon standard double clamp used between TRSV and Hanger (SAP: 372272)			
				End of string including calculated stretch (m):				0	1x Cannon Special cable clamp above TRSV (SAP: 477984)			
WELL SCHEMATIC		ITEM NUMBER	DESCRIPTION	LENGTH (m)	TOP ITEM (mBRT)	ID (inches)	OD (inches)	THREAD	MODULE No. Joints	SUPPLIER	Volume (bbl)	
			Correction for RTE (Workover only)		0.0							
		1	Tubing Hanger below HOP Part Number: 218340-04-02 Serial Number: HME000	0.250	8.92	6.276	14.080	Vam Top B	Thighanger	Cameron	0.0	
		2	7" Pup Joint, 26ppf, 13Cr, L80	1.589	9.17	6.276	7.677	Vam Top BxP		Cameron	0.2	
		3	7" Tubing, 26ppf, 13Cr, L80	12.029	10.76	6.276	7.677	Vam Top BxP	1	ISG	1.7	
		4	7" Pup Joint, 26ppf, 13Cr, L80	1.724	22.79	6.276	7.677	Vam Top BxP	1	ISG	2.0	
		5	7" Pup Joint, 26ppf, 13Cr, L80	3.096	24.51	6.276	7.677	Vam Top BxP	1	ISG	2.3	
		6	7" Tubing, 26ppf, 13Cr, L80	36.102	27.61	6.276	7.677	Vam Top BxP	3	ISG	6.9	
		7	7" Pup Joint, 26ppf, 13Cr, L80	3.100	63.71	6.288	7.587	Vam Top BxP		ISG	7.3	
		8	7" Flow Coupling, 13Cr, L80, 26ppf. Part Number: 428758 Serial Number: 19124533	1.780	66.81	6.221	7.603	Vam Top BxP		Halliburton	7.5	
		9	TRSV, SP Valve, 7", Self Equalizing, 13Cr With 5.963" RPT™ Internal Lock Profile Part Number: 10141293 Serial Number: 1937674-1	3.283	68.59	5.963	9.231	Vam Top BxP		Halliburton	7.9	
		10	7" Flow Coupling, 13Cr, L80, 26ppf. Part Number: 438983 Serial Number: 1855554	1.782	71.87	6.258	7.606	Vam Top BxP		Halliburton	8.1	
		11	7" Pup Joint, 26ppf, 13Cr, L80	1.939	73.66	6.289	7.579	Vam Top BxP		ISG	8.3	
		12	7" Tubing, 26ppf, 13Cr, L80	1697.097	75.59	6.276	7.677	Vam Top BxP	132	ISG	221.4	
		13	X-over, 7" 26ppf x 5" 15ppf, 13Cr, L80	0.512	1772.69	4.408	7.677	7" Vam Top Bx 5" Vam Top P	1	ISG	221.4	
		14	5" Tubing, 15ppf, 13Cr, L80	779.660	1773.20	4.276	5.577	5" 18M VTBxP	65	ISG	266.8	
		15	5" Pup Joint, 15ppf, 13Cr, L80	2.930	2552.86	4.423	5.481	Vam Top BxP		ISG	267.0	
		16	Ratchet-Latch Locator SSR (Rotaretorelease Latch) Part Number: 10137 Serial Number: 2340702-08	0.740	2555.79	3.956	5.484	Vam Top B		Halliburton	267.0	
		17	7/23-32# MHR Packer, 13Cr Part Number: 10148148 Serial Number: 2447072-08	1.815	2556.53	3.930	5.857	New VAMB, 5" 18ppf		Halliburton	267.1	
		18	Reducing Adapter, 5" 18ppf New Vam x 5" 15ppf Vam Top, 13Cr Part Number: 141837 Serial Number: 2278088	0.155	2558.35	4.273	5.018	New VAM 5" 18ppf Vam Top P		Halliburton	267.1	
		19	5" Pup Joint, 15ppf, 13Cr, L80	1.869	2558.50	4.472	5.483	Vam Top BxP		ISG	267.3	
		20	5" Tubing, 15ppf, 13Cr, L80	11.969	2560.37	4.408	5.470	Vam Top BxP	1.0	ISG	268.0	
		21	5" Pup Joint, 15ppf, 13Cr, L80	2.985	2572.34	4.380	5.448	Vam Top BxP		ISG	268.2	
		22	3.813" RN Landing Nipple Part Number: 13731 Serial Number: 2297261	0.400	2575.33	3.813	5.525	Vam Top BxP		Halliburton	268.2	
		23	5" Pup Joint, 15ppf, 13Cr, L80	1.914	2575.73	4.439	5.457	Vam Top BxP		ISG	268.3	
		24	5" Tubing, 15.0ppf, 13Cr, L80, R3	11.979	2577.64	4.408	5.470	Vam Top BxP	1.0	ISG	269.1	
		25	5" Pup Joint, 15ppf, 13Cr, L80	2.925	2589.62	4.397	5.468	Vam Top BxP		ISG	269.2	
		26	3.813" RN Landing Nipple Part Number: 13731 Serial Number: 2297262-07	0.415	2592.54	3.725	5.525	Vam Top BxP		Halliburton	269.3	
		27	5" Pup Joint, 15ppf, 13Cr, L80	2.044	2592.96	4.398	5.459	Vam Top BxP		ISG	269.4	
		28	5" Tubing, 15.0ppf, 13Cr, L80, R3, c/w 1/2 mud shoe	8.000	2595.00	4.408	5.000	Vam Top BxP	1.0	ISG	269.9	
		29	Bottom of String		2603.00							
		29	Polished Bore Receptacle 7"x5" 20-35# PBR	3.450	2600.80	5.710	5.775			Weatherford	0.4	
		30	Liner Top Packer-CTSP4R 7"x5" 29-32#	1.590	2604.25	5.870	5.920	Vam Top P		Weatherford	0.5	
		31	Seat Stem	0.980	2605.84	5.220	5.930	Vam Top BxP		Weatherford	0.6	
		32	Polished Bore Receptacle 7"x5" 20-35# PBR	5.000	2606.90	3.958	4.937			Weatherford	0.2	
		33	Liner Top Packer-CTSP4R 7"x5" 29-32#	1.080	2611.90	4.330	5.910	Vam Top P		Weatherford	0.3	
		34	Hydraulic Non Rotating Liner Hanger Assy. CTH	1.610	2612.98	4.330	5.910	Vam Top BxP		Weatherford	0.4	
		35	5" Tubing, 15.0ppf, 13Cr, L80, R3	13.022	2614.59	4.408	5.470	Vam Top BxP	1.0	ISG	1.2	
		36	5"x-overpup joint, 15ppf, L80	2.940	2627.61	4.408	5.470	5" Vam Top B 4x5" New Vam P		ISG	1.4	
		37	Flapper Valve (KOI), L-80, 13Cr Part Number: 8126CF7605-F / 1017527605 Serial Number:	0.830	2630.55	3.502	4.937	5" Vam Top Bx 4x1/2" Vam Top P		FV-1	Halliburton	1.4
38	4.5"x-over joint, 12.6ppf, L80	1.950	2631.38	3.958	4.960	Vam Top BxP		ISG	1.5			
39	4.5" slotted liner, 12.6ppf, L80 Note: 4.5" Stinger Packoff at 3014m, ID1.50".	160.500	2633.33	3.958	4.960	Vam Top BxP		ISG	9.5			
	Bottom of String/w Guide Shoe		2793.83									

Initial:
Ozgu Ozbay 26/10/2012 Updated: Ju de Eron mwon 05/11/201

III.6.2 Suspension Schematic

Rig Name: KCAD
 T220RTE: 9.15m
 RTE to hangoff point: 9.39

Note: All depths referenced to KC
 D220RTE=9.15m AGL

Well Data:

Hole Size	Depth (m DDbrt)
24"	77
17-1/2"	910
12 1/4"	1868
8 1/2"	2874
6"	2999

Casing	Depth (m DDbrt)
30"	5.0
18 1/2"	76.8
13 3/8"	908.0
10 3/4" x 9 5/8" CrossOver	91.0
9 5/8"	1865.0
7" Liner PBR Top	1794.0
7" Liner Shoe	2868.0
4 1/2" Slotted Liner PBR Top	2606.9
4 1/2" Slotted Liner Shoe	2793.8

Completion Summary:

	Depth (m DDbrt)
7" TRSV	68.6
5.963" RPT Profile on TRSV	68.6
X-over 7"x5"	1772.7
Ratchet Latch-Rotate Type	2555.8
7" MHR Packer	2556.5
3.813" R Nipple	2575.3
3.813" RN Nipple	2592.5
Bottom of 5" Tubing	2603.0

Reservoir Isolation

Flapper Valve	2630.6
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Suspension Details:

TRSV closed
 BPV set in tubing hanger

Reservoir Sections

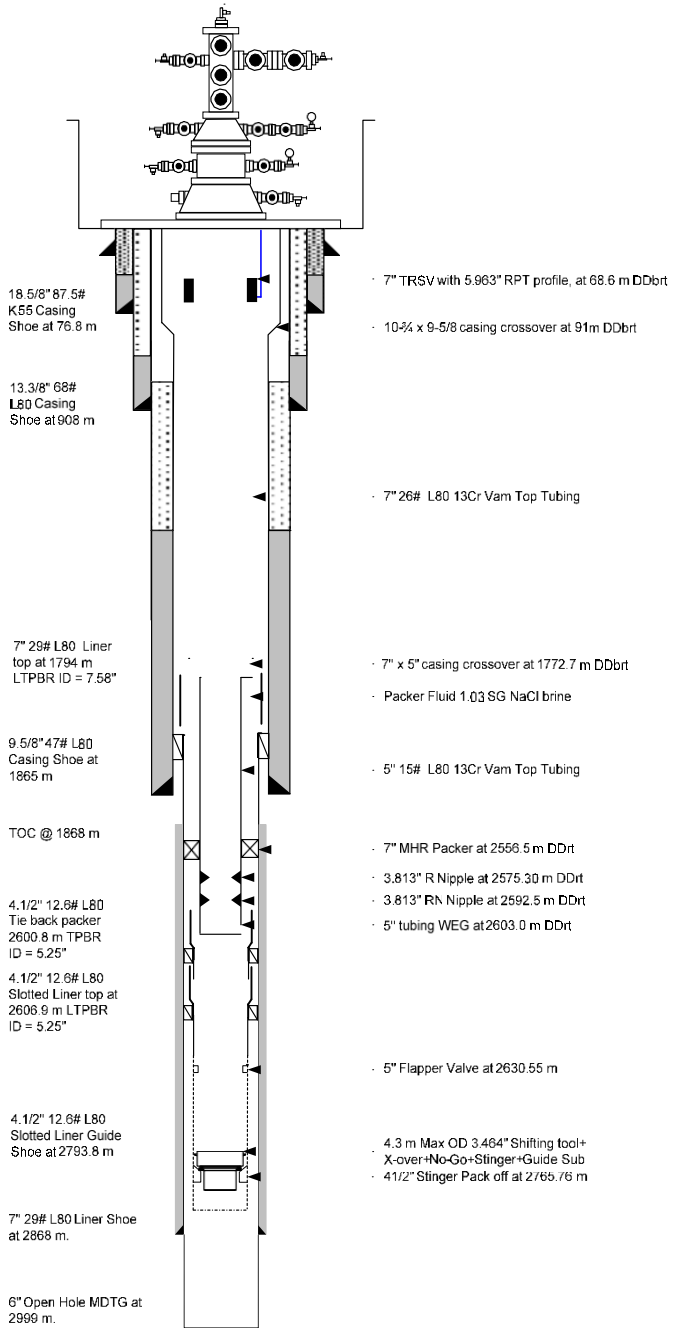
Lower D40	Top	2937.5 m DDbrt
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Reservoir conditions at top of reservoir

D40	
Pressure	2317 Psia TBC
Temperature	144°C

Initial: Ozgur Ozbay
 26/10/2012 Updated: Jude Eronmwon0
 5/11/2012

Teg-37
Suspension Schematic Fina



III.7. JOBPARAMETERS :**III.7.1. Wellbore Teg-37 :**

Tubing1	0ft	to 5,816ft	7"	X	26	PP	X	6.276"ID
						F		
Tubing2	5,816ft	to 8,553ft	5"	X	15	PP	X	4.408"ID
						F		
Casing	0ft	to 6,119ft	9-5/8"	X	47	PP	X	8.681"ID
						F		
Liner	8,553ft	to 9,840ft	4 1/2"	X	12.6	PP	X	3.958"ID
						F		
Packer	8,388ft							

III.7.2. Reservoir :

EstimatedReservoirPressure(D40)

2,19

5 psiEstimatedReservoirTemperature(D40)

291

Deg.F.FracGradient,(Estimated)

0.75

psi/ft

FracPressureatMidofLiner 7,219

psiHydrostaticPressureoffluidinwell(0.41psi 346

psiMaximumWellheadPressure Basedonthe

fluidinthewell

MaximumCoiledTubingPressure 5,000psiEquipmentLimitation

III.7.3 Fluids :

FreshWater 1,389gals

Nitrogen 7m3

FreshWater requiredfortheoperationwillbesuppliedbyclient

III.7.4 Equipment Required :

1ea. 1-1/2" x 0.109" Wall Thickness, QT - 900
Coiled Tubing Unit
1ea. Clam Mixing Unit with HT-
400 Pump

1ea. Nitrogen Pumping Unit with 10 m³
N₂ storage tank
1ea. 26m³ Nitrogen transport

III.7.5.BHA :

1ea Service Connector

1ea Double Flapper Check Valve

1ea Hydraulic Disconnect

1ea Knuckle Joint

1ea 1 Meter Strait Joint

1ea Wash Nozzle

III.8. JOBPROCEDURE :

Table III.2 : job procedures Represents

Teg-37: Well Unloading								
Stage No.	Stage Volume (bbl)	Fluid	Stages Description	Stage Clean Volume (gals)	Stage N 2 Volume (liters)	Total Clean Rate (bpm)	Stage Time (min)	Job Time (min)
1			Conducts safety meeting, ensure involved people and company man are present.				15 min	15 min
2			Rig up CT , pumping & N2 units, Rig up surface lines to CT Function test BOP. (See Note #5 below).				100 min	115 min
3	25	Fresh Water	Fill coiled tubing and surface lines with Fresh Water for pressure testing.	1,039		1.20	21 min	136 min
4		Nitrogen	Cool down Nitrogen unit.		1,000			136 min
5	2	Fresh Water	Pressure test CT against swab valve and N2 pumping lines separately to 500/4000 psi for 5/10 mn respectively.	100			45 min	181 min
6	6	Fresh Water	Open Swab valve, Open wing valve and circulate to see fluid returns	250		1.20	5 min	186 min
7		Nitrogen	Use N2 to Displace Fresh Water from CT to the flare pit		600		20 min	206 min
8			Open well (make sure TRSSV is open) and start RIH at 20 fpm until pass the TRSV (68.6 m/225 ft) .				11 min	217 min
9			Continue RIH to 2,300m @ 65 fpm , safer running speed without pumping N2. Perform check weight every 2,000ft .				116 min	333 min
10		Nitrogen	Continue RIH to 2,745m @ 30 fpm while pumping N2 at 20l/mn		973		49 min	382 min
11		Nitrogen	Stop CT at 2,745m , Pump 0.5m³ of liquid Nitrogen at high rate (40-60 lpm)		500		10 min	392 min
12		Nitrogen	Slow down nitrogen rate to the 20-25 lpm, make sure all the fluid above this depth has been displaced, until only N2 observed on surface.		800		40 min	432 min
13		Nitrogen	Continue pumping Nitrogen at 20-25 lpm, until well starts to flow and can sustain the production on its own. Adjust nitrogen rate if needed.		1,000		33 min	465 min
14		Nitrogen	POOH to surface, while maintaining N2 circulation at minimum rate 15 lpm if needed.		1,350		90 min	555 min
15			Close the swap valve, secure the well and rig down injector.				60 min	615 min
16			Leave the well flowing for cleanup.					615 min
Totals	33.1 bbl			1,389	6,223			10.2 hrs

Note

- 1) The well needs to be equipped with a flare line and an adjustable choker running as a safe distance from the well.
- 2) The above is a guideline. Adjust rates & volumes as needed to suit the job requirement.
- 3) Attempt to stabilize N2 rate and CT speed to unload the well fluid at 500 scf/bbl
- 4) The chokes should be properly adjusted to maintain back pressure in the well and avoid excessive drawdown
- 5) Plant to perform off-line the following test: pigging CT, pressure tests of blind and pipe rams.

III.9. Procedure :

1. Conduct safety meeting, ensure involved people and company man are present.
2. Rig up CT, pumping & N₂ units, Rig up surface lines to CT Function test BOP. (See Note #5 below).
3. Fill coiled tubing and surface lines with Fresh Water for pressure testing.
4. Cool down Nitrogen unit
5. Pressure test CT against swab valve and N₂ pumping lines separately to 500/4000 psi for 5/10 mn respectively.
6. Open Swab valve, Open wing valve and circulate to see fluid returns
7. Use N₂ to Displace Fresh Water from CT to the flare pit
8. Open well (make sure TRSSV is open) and start RIH at 20 fpm until pass the TRSV (68.6m/225ft).
9. Continue RIH to 2,300 m @ 65 fpm, safe running speed with out pumping N₂.
Perform check weight every 2,000ft.
10. Continue RIH to 2,745m @ 30 fpm while pumping N₂ at 20l/mn
11. Stop CT at 2,745m, Pump 0.5m³ of liquid Nitrogen at high rate (40-60lpm)
12. Slow down nitrogen rate to the 20-25lpm, make sure all the fluid above this depth has been displaced, until only N₂ observed on surface.
13. Continue pumping Nitrogen at 20-25lpm, until well starts to flow and can sustain the production on its own. Adjust nitrogen rate if needed
14. POOH to surface, while maintaining N₂ circulation at minimum rate 15lpm if needed.
15. Close the swab valve, secure the well and rig down Injector.
16. Leave the well flowing for cleanup.

III.9.1 Note:

- 1- The well needs to be equipped with a flare line and an adjustable choker running a safe distance from the well.
- 2- The above is a guideline. Adjust rates & volumes as needed to suit the job requirement.
- 3- Attempt to stabilize N₂ rate and CT speed to unload the well fluid at 500 scf/bbl .
- 4- The chokes should be properly adjusted to maintain back pressure in the well and avoid excessive drawdown .

III.10. CTBOTTOMHOLEASSEMBLY:


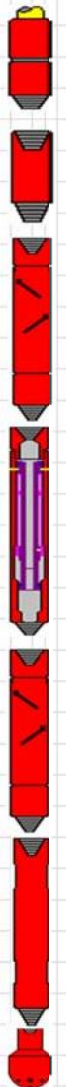
		STANDARD WASH BHA SCHEMATIC					
Customer:	JV-Gas	Customer Rep:					
Field:	ISG	Well Type:	Gas				
Well Nos:	Teg-37	HES Rep/s:					
Rig Type:		HES Office:					
Installation:		Service Order:					
Location:	In Salah/ khrechba	DATE	September 11, 2013				
Tool String	Item Nos	O.D. (inches)	I.D. (inches)	Length (Inches)	Description of Item	Top Conn	Bottom Conn
	1	1.750		1.50	Roll on connector		
	2	2.000		4.75	Bump Sub		
	3	1.700	0.72	10.50	Double Flapper Valve		
	4	1.810	0.54	12.00	Hydraulic Disconnect		
	5	1.760	0.50	15.50	Knuckle Joint		
	6	1.690		23.75	Straight Bar		
	7	2.000		6.00	Wash Nozzle		
				74.00 in			

Figure III.6:Standard wash BHA schematic

Note: All lengths and O.D.s need to be checked and noted before running the BHA.

III.11.RIGLAYOUT :

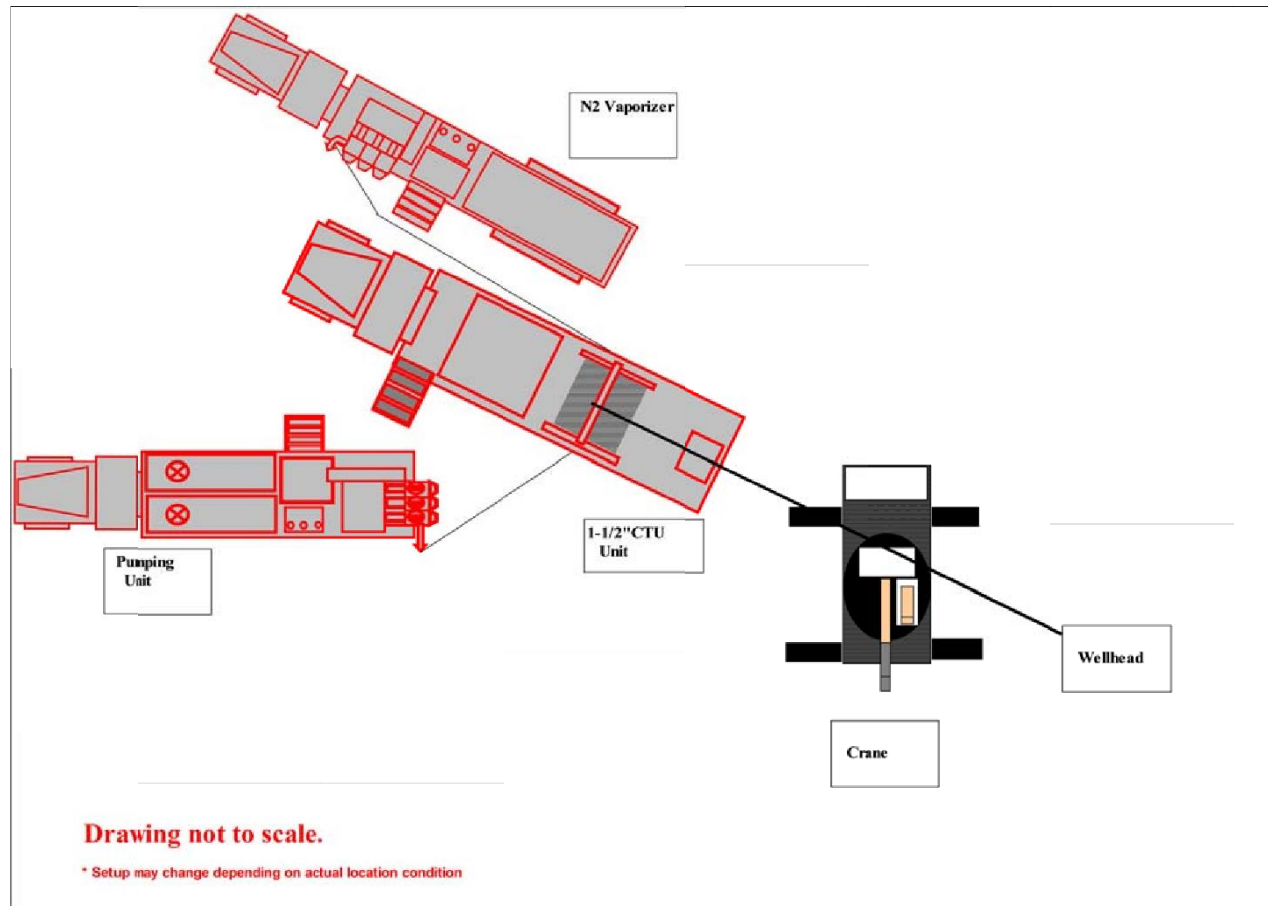


Figure III.7 :RigLayoutRepresents

III.12.STACKUPDIAGRAM :

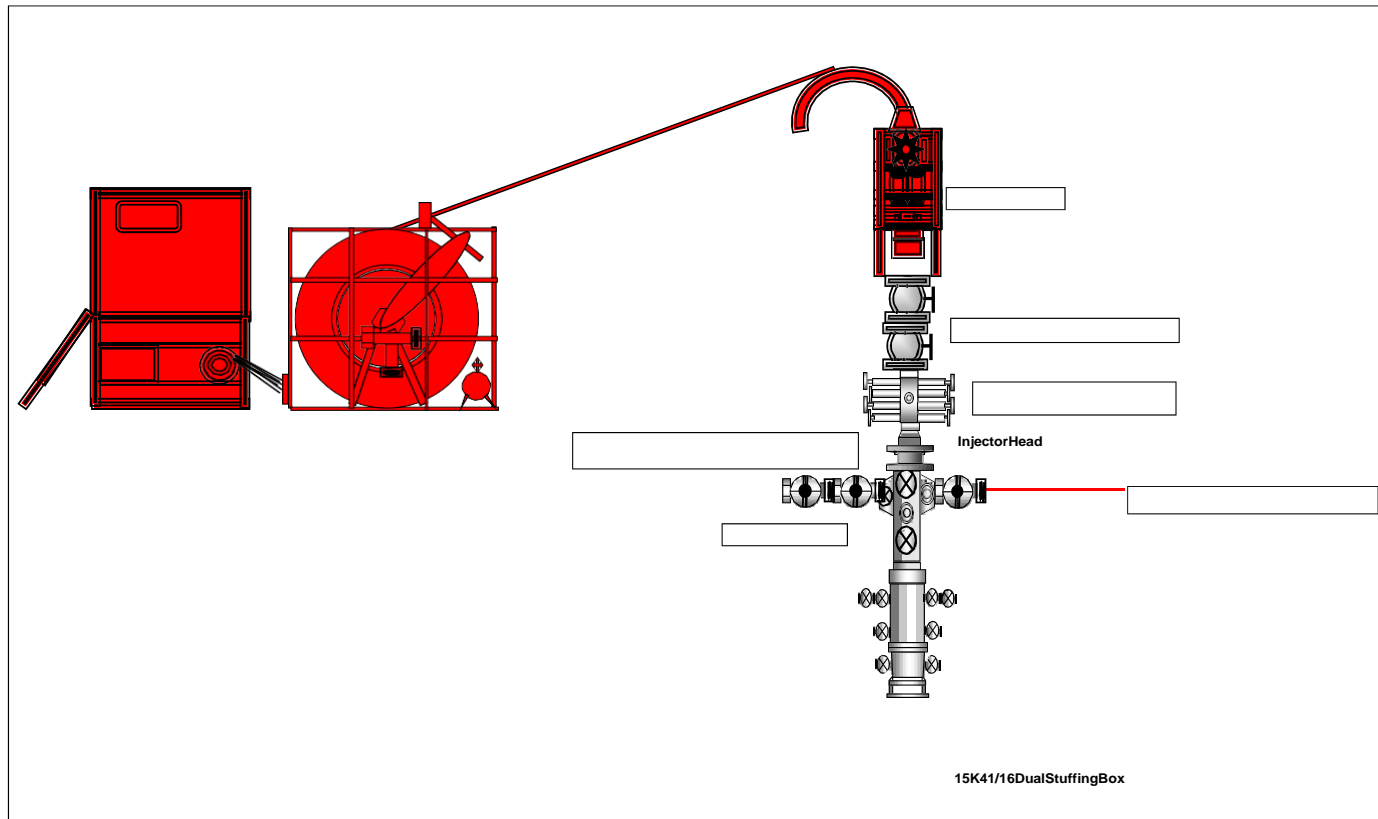


Figure III .8 :STACKUPDIAGRAM

III.13. Slick Line and Clean Up Operations step by step :

III.13.1. Day 1: Slick Line WORK :

Drifting To Total Depth (HUD) :

- With the well shut-in at the choke and manual wing valve, make up a 3.3 “ sized tubing drift/gauge (1-3/4” CT will be used in N2 lift), and attach to the wire line tool string.
- Connect the lubricator, and pressure test.
- Open the UMV. Slowly open the Swab Valve (SV) to expose the lubricator assembly to full well pressure. Note the shut-in tubing pressure.
- When 5 m below DHSV POOH slowly to confirm DHSV is open. If hanging up stop and evaluate. Cont to RIH to establish HUD. POOH
- Take note of any restrictions or over pulls encountered while making the drift run in the well.
- Close UMV and SV on Xmas Tree, bleed-off pressure, break lubricator and remove the drift tool, Inflow test / tree valves and grease if needed.

III.13.2. Day 2 :RU of Schlumberger Test Equipment :

Well Test Equipment Rig-up :

- Obtain a work permit prior to commence the job.
- Prior to any operations hold a safety meeting with all personnel involved, and ensure that all safety signs are in position and well test area is enclosed by barrier tape.
- Ensure the manual production wing valve, UMV and LMV is locked in the closed position.
- Rig up the Schlumberger ESD to hydraulic WSSV.
- Rig up Schlumberger surface test equipment to Schlumberger ESD and out to the flare pit.
- Ensure to avoid 90 degrees elbows in the rig-up as much as possible to avoid unnecessary erosion. It is particularly important not to have an elbow on the outlet of

the choke manifold The flare line should be chocked up so it can be screwed straight onto this outlet.

- All lines to choke manifold tested to 3500 psi. And all lines down stream the manifold must be tested to 1200 psi .And the area must be cleared when that pressure test is ongoing.
- Ensure that there are no intrusive probes in any of the upstream or downstream lines (thermo wells, etc) especially during the clean-up period. Rocks can damage these probes and cause leaks if not sealed in. Any intended in-line probes in the lines must only be inserted after the well has been cleaned up, Risk Assessed, and ensured to have a positive and rated pressure seal (needle valve, gauge, etc).

 **PRESSURE TEST EQUIPMENT :**

- Move in rig up Schlumberger pump unit
- Get 2 radios to communicate between pump operators and well test chief operator.
- Barrier off area.
- Discuss test procedure with pump operator and all the other personnel involved highlighting risks.
- Make sure all valves to flare are open before flushing lines.
- Start flushing lines at pumping rate of 1.5 bbl/min with centrifuge pump. Once clear returns are observed at flare line end, stop pumping.
- Install 6” 206 Test plug on flare line with valve on test plug open.
- Flush again lines at low pumping rate with centrifugal pump.
- Stop flushing and isolate flare line (close valve on test plug).
- From SLB Unit apply 300/1200 for 5/10 min. (Record all pressure test on chard recorder)
- Close downstream valves on choke manifold.
- Bleed off at the 6” test plug at flare end and remove plug.
- Confirm to pump operator that the pug has been removed.
- Apply 300/3500 for 5/10 min against downstream valves on choke manifold.
- Close upstream valves on choke manifold.
- Open downstream valves.

- Apply 300/3500 for 5/10 min against upstream valves on choke manifold.
- If the pressure test passes, bleed off pressure from surface lines and secure the well area before leave the well.

III.13.3.Day 3: Coiled tubing Rig Up and Unloading the Well:

Check weather forecast for the well location for the time period when hydrocarbons will be first produced to surface. If acceptable weather conditions are anticipated for the beginning of the test, proceed with the test programme. Unacceptable conditions are high winds particularly ones blowing toward rig, blowing sand, and low visibility.

- Ensure to have a valid flaring permit in place before commencing the job, Inform the OLC and the military prior to start the flare.
- Carry out gas check prior to moving CT unit to the well.
- Confirm tree valve status.
- Spot and rig up the CT unit and associated equipment as per HES's standard operating procedures and JVGAS regulations.
- Prepare N2 equipment.
- M/U BOP and CT nozzle (CT tools string composed by, Roll on Connector 1.75", Bomb Sub 2", Dual Flapper check valve 1.7" , Hydraulic disconnect 1.81", Straight bar 1.69", Wash Nozzle 2").
- Ensure hydraulic disconnect will work if needed to release CT and also use an appropriate bull size.
- P/T to 500/4000psi for 5/10 minutes for CT PCE and surface lines..
- Open TRSSSV using Enerpac hand pump. Keep it open at 300 to 320 bars.
- Open Swab valve and UMW. Record WHP.

Ensure that the TRSSSV is kept open all the time when CT is down hole..

- Start RIH. Take extra care when running through X-mas tree valves and TRSSSV. Once through TRSSSV come on line with N2 at minimum rate. Get weight. checks every 500 m while RIH
- Open the well at choke manifold on adjustable choke (128/64") to flare pit.
- RIH with the Coiled Tubing not faster than 6 m/min.

Visually inspect the line-up from the tree to the burners and check that all valves are in the correct position. The Intervention Supervisor and the Well Test Supervisor should witness this.

-
- Once clear of the TRSSV increase RIH speed to 15 to 20 m/min and start pump N2 at minimum rate, When at depth below 2500 m, start injecting nitrogen at a minimum of 500 scf/min
 - Insure that “A” and “B” annulus are monitored during the flow period to ensure they do not exceed maximum allowable pressures, No more then 500 psi.
 - Conduct pull test every 250 m and compare weights with calculated weights. Slow down running speed going through the landing nipples and the top of liner, returns are to be taken to the flare pit. Monitor fluid returns closely for any signs of gas, Ensure that the pilots are lit.
 - Continue RIH in steps of 250 m each parking the coil for 5/10min maintaining nitrogen rate at 500 scf/min until the well starts flowing or until the end of the coiled tubing is at 2745 m (Last HUD-10 m), continue to pump nitrogen until the hydrocarbon liquid (Top of hydrocarbon liquid proximately 2500 m)has been displaced with nitrogen.
 - N2 has to be shut in prior to closing the well for the not frac the formation,
 - Once it is confirmed that the well will flow without N2, POOH with CT into the lubricator and close the Swab valve. Clean up the well at the highest rate possible and at lowest possible FWHP
 - Monitor the flow line for signs of erosion, especially if solids are produced. Record Ultrasonic thickness measurements.
 - If there is any indication of flow line erosion, well must be secured and lines have to be opened and inspected.
 - Flow the well until all of the hydrocarbon liquid has been flared
 - The length of the clean up period is a judgment call of the well site OPS Intervention Supervisor.
 - Bleed off and maintain annulus pressure below 500 psi during the clean up. Record the volume and type of fluids recovered and report on the OPS daily report and Well test report.
 - Obtain pressures at various choke settings with estimated flow rate at the Data Acquisition Unit, and reported in well test reporting.
 - Obtain condensate gas ratio (CGR) measurement in the end of the clean up operation.

III.14.4.Day 4: Rig Down of Well test equipments :

This step is to be done after confirming the well is cleaned up and not necessary in the 4th day .

- With the UMV, Manual Wing Valve, Actuated Wing Valve, and Kill wing closed, open the swab valve and bleed down the pressure through the choke manifold and inflow test of tree-x.
- Open the kill wing valve keep all valve closed and flush the Schlumberger test equipment with fresh water.
- Rig down ESD from the WECO connection. necessary
- Rig down Schlumberger test equipment.
- Open the kill wing valve to bleed any trapped pressure and then close it again.
- Remove the 2-1/16” flange x 2” 1502 WECO from the kill wing.
- Pressures test the companion flange to 5000 psi with a hydraulic hand pump against the kill wing valve.
- With the Wing Valve, Actuated Wing Valve, and Kill wing closed, open the swab valve and close the swab needle valve.
- Function test of WSSV and close it
- Slowly open the UMV to test the tree cap installation, the tree cap flange and cap needs to be tested to 5k. All pressure tests should be recorded and retained.
- Close the UMV and bleed off the pressure above the UMV through the swab needle valve.
- Close the swab valve..
- After rig down of all equipment, check the site to verify it is as clean as before the operation.
- Notify the Area Authority and Teg Operations Superintendent that the cleanup is complete and sign off on the permit.

III.15.CALCULATIONS :

III.15.1.Weight of Gas Column to 2500 m (Top of hydrocarbon liquid) :

- WHP = 85 bars (1232 .5 psi)
- Correction factor for gas with SG : $0.628 = 1.181$
- $HP = 1.181 \times 1232,5 = 1456 \text{ psi}$

III.15.2.Weight of Hydrocarbon liquid from 2500 m to (HUD – 10 m) :

- Hydrocarbonliquid gradient = 0.4 psi / ft
- HUD = 2757 m
- $HP = 0.4 \times (247 \times 3.28) = 324 \text{ psi}$

Total weight of Gas column and hydrocarbon column to (HUD – 10 m) = $324 + 1456 = 1793 \text{ psi}$.

III.15.3.Wight of hydrocarbon column from (HUD – 10 m) to top perforation (at 2930 m) :

- Length of the hydrocarbon column = $2930 - 2747 = 183 \text{ m}$
- $HP = 0.4 \times (183 \times 3.28) = 240 \text{ psi}$.

III.15.4.Total weight of Wellbore fluid column to top perforation (at 2930 m) :

Total weight = $240 + 324 + 1456 = 2020 \text{ psi}$.

- Reservoir pressure = **1961 psi** (June 2012) (From SOR of Teg-37).
- Bottom hole pressure at Gauge depth (at 2750 m WL) = **1848 psi** (*Pressure Gradient Surveys Job on the 27/04/2013*).

III.16.Diagrams and Scenario Schematics:

III.16.1.1st Scenario: 55 mmscf/d (Shlumberger Simulation) :

2 Well Test Layout

2.1 Pfd Drawing

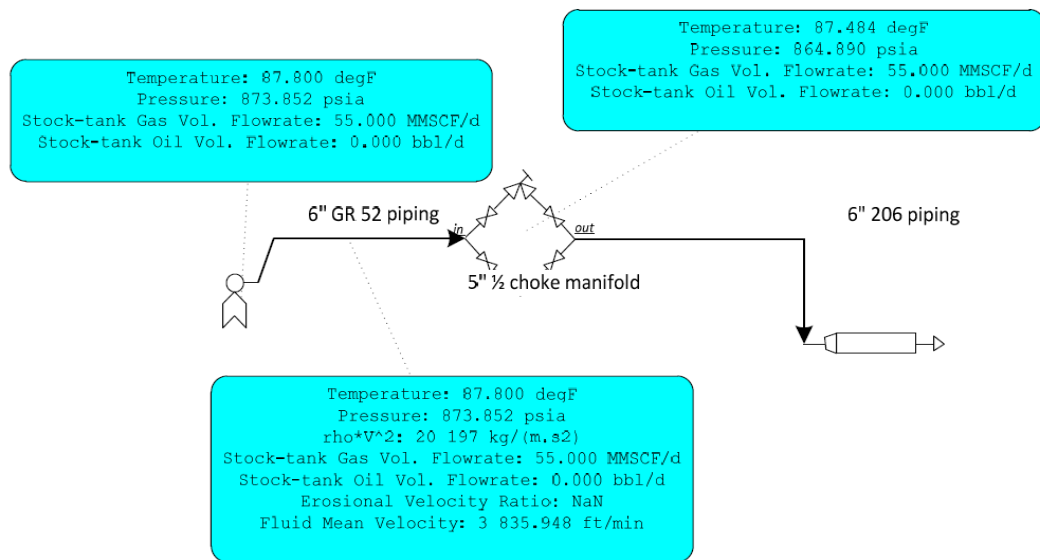


Figure III .9: Scenario well test Layout 1

III.16.2.2nd Scenario : 14 mmscfd (Shlumberger Simulation) :

2.1 Pfd Drawing

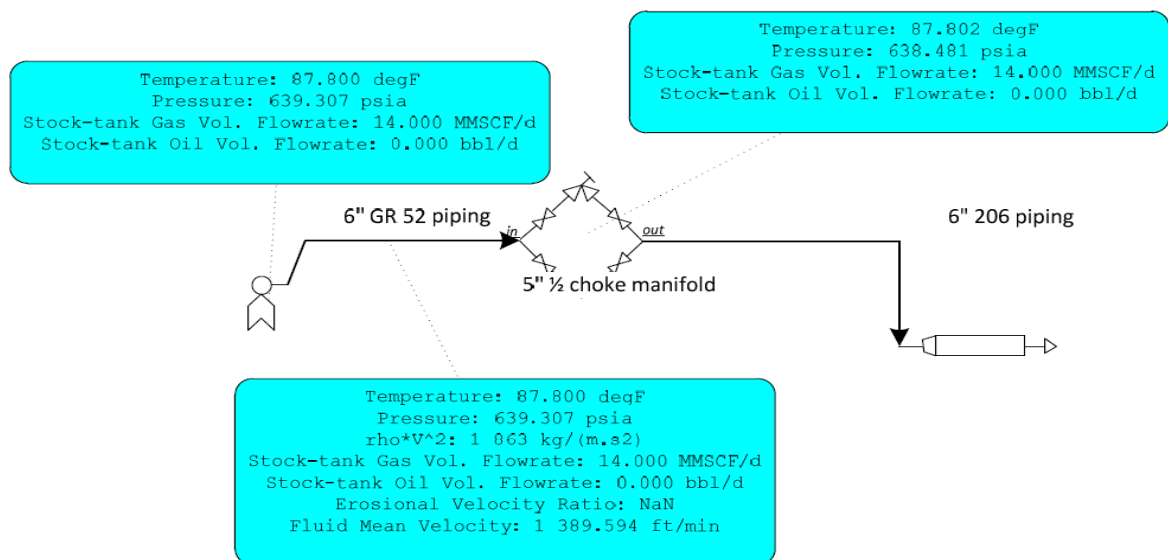


Figure III .10 : Scenario well test Layout 2

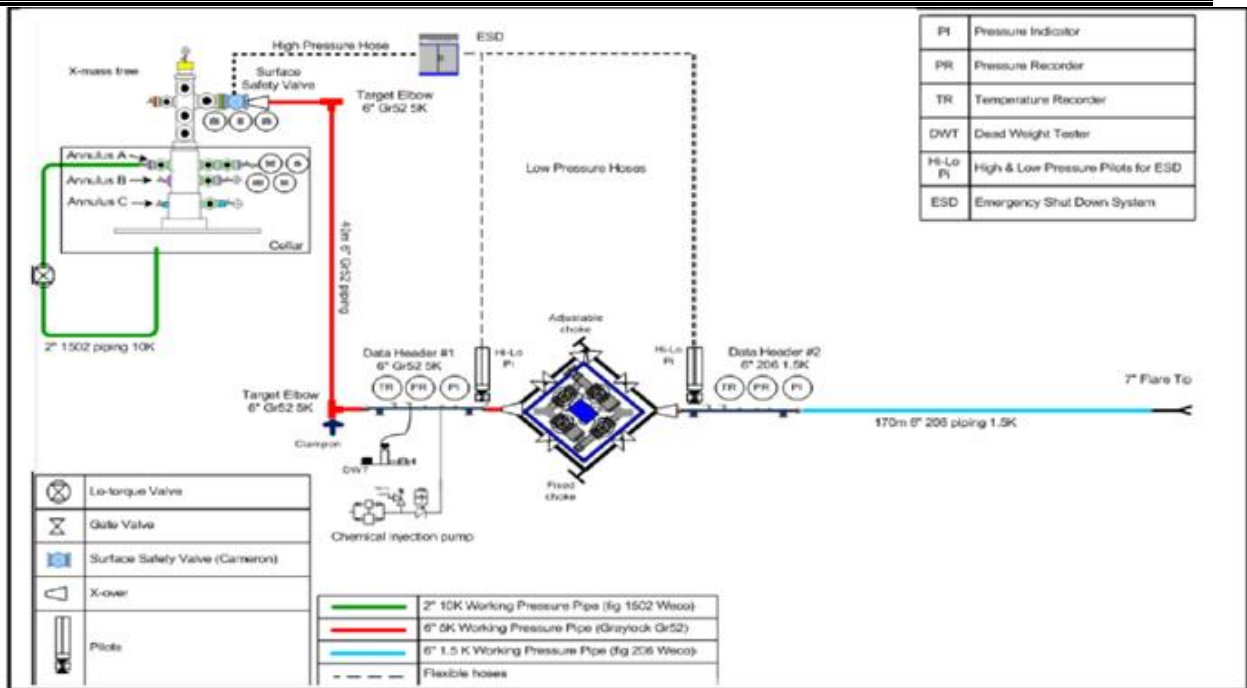


Figure III.11 : surface testing equipment layout

III.17. conclusion :

In each case study couled tubing is used to solve the problems posed or to maintain the well and to save the production but in the other cases we will change the parameters of well operations as another hole layer link is created. and all these interventions are successful without problem but each operation is expensive so the transition after the problem creates continuity in productivity .

Reservoir pressure is less then column weight by about **60 psi**.

CT and Clean up will be able to reduce bottom hole pressure by 324 psi maximum from the 2020 psi (Total weight of the column in the Wellbore to top perforation.

Conclusion General

ConclusionGeneral :

According to the present study and before highlighted the importance and the effectiveness of the couled tubing interventions the wells, with all the advantages to the intervention on the wells is production. Among the advantages can be Technological development in terms of dealing with problems. impede production processes (Tools and calves treatment programs and the establishment of modern processes to restore, protect and increase productivity, New chemicals more effective than those currently used

- ✓ multiesed tool multiesmultized in the same process increases the success rate
- ✓ Specific transition between interventions due to specific problems of some disadvantages such as
- ✓The development of the mechanism used in the interventions creates a price increase
- ✓ Different techniques of intercreation of hemutations of result options of multivariate of the multifier several new products chSimiques creates new problems that cannot be solved
- ✓The disruption of safety during new interventions in the pilot phase of the primary

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